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(54) Title: VANADIUM OXIDE PARTICLES AND BATTERIES WITH ELECTROACTIVE NANOPARTICLES

(57) Abstract

Vanadium oxide nanoparticles with different vanadium oxidation states and different crystal structures. The particles have a narrow distribution of particle diameters and unique properties that result from their small size and correspondingly large surface area. The particles are produced by laser pyrolysis, and can be further treated to change their properties, without destroying their nanoscale size. The stoichiometry and crystal structure can be varied by initial heating under mild conditions. The materials may be used as cathode active materials in high energy density batteries.

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## VANADIUM OXIDE PARTICLES AND BATTERIES WITH ELECTROACTIVE NANOPARTICLES

### FIELD OF THE INVENTION

The invention relates to nanoscale vanadium oxide particles. The invention further relates to the production of nanoscale vanadium oxide particles using laser pyrolysis and the conversion of the stoichiometry and/or crystal structure of vanadium oxide particles by applying heat. The invention further relates to batteries, especially lithium batteries and lithium ion batteries, incorporating nanoparticles, such as vanadium oxide nanoparticles, as an electroactive material.

### BACKGROUND OF THE INVENTION

Vanadium can exist in various oxidation states. Correspondingly, vanadium oxides are known to exist with various stoichiometries. In addition, vanadium oxides with a particular stoichiometry can have various crystalline lattices, or they can be amorphous. Thus, vanadium oxides exhibit an extraordinarily rich phase diagram.

Vanadium oxides with various stoichiometries have been noted as promising materials for use in lithium based batteries. Appropriate vanadium oxides can intercalate lithium ions into their crystal structure. In addition, vanadium oxides are useful in a variety of other applications, for example, as catalysts for chemical reactions. Because of the interest in vanadium oxides, several approaches have been developed for producing vanadium oxides.

The microminiaturization of electronic components has created widespread growth in the use of portable electronic devices such as cellular phones, pagers, video cameras, facsimile machines, portable

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stereophonic equipment, personal organizers and personal computers. The growing use of portable electronic equipment has created ever increasing demand for improved power sources for these devices. Relevant 5 batteries include primary batteries, i.e., batteries designed for use through a single charging cycle, and secondary batteries, i.e., batteries designed to be rechargeable. Some batteries designed essentially as primary batteries may be rechargeable to some extent.

10 Batteries based on lithium have been the subject of considerable development effort and are being sold commercially. Lithium based batteries generally use electrolytes containing lithium ions. The anodes for these batteries can include lithium metal (lithium batteries), or compositions that intercalate lithium (lithium ion batteries). Preferred electroactive materials for incorporation into the cathodes are compositions that intercalate lithium. The compositions that intercalate lithium, for use in the cathodes, 15 generally are chalcogenides such as metal oxides that can incorporate the lithium ions into their lattice. Vanadium oxides are examples of promising compounds for the production of cathodes because of their high theoretical energy densities..

20 25 SUMMARY OF THE INVENTION

In one aspect, the invention features a collection of particles including vanadium oxide, the measurements along the principle axes of the particles are each about 1000 nm or less for at least about 95 30 percent of the particles. The particles have an average diameter of generally about 1000 nm or less, preferably about 150 nm or less, more preferably from about 5 nm to about 100 nm, and even more preferably from about 5 nm to about 50 nm.

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The vanadium oxide nanoparticles can have a stoichiometry, for example, of  $\text{VO}_2$ ,  $\text{V}_2\text{O}_5$  or  $\text{V}_6\text{O}_{13}$  and can be amorphous or crystalline. Preferably, about 95 percent of the vanadium oxide nanoparticles have a diameter greater than about 50 percent of the average diameter and less than about 150 percent of the average diameter.

In another aspect, the invention features a method of producing vanadium oxide nanoparticles including the step of pyrolyzing a molecular stream including a vanadium precursor, an oxidizing agent and a radiation absorbing gas in a reaction chamber, where the pyrolysis is driven with heat absorbed from a laser beam. The vanadium oxide nanoparticles preferably have an average diameter from about 5 nm to about 150 nm. The laser beam preferably is produced by  $\text{CO}_2$  laser. The radiation absorbing gas can include  $\text{C}_2\text{H}_4$ . The vanadium precursor can include  $\text{VOCl}_3$ , and the oxidizing agent can include  $\text{O}_2$ .

In another aspect, the invention features an apparatus including:

- (a) a reaction chamber isolated from the ambient atmosphere;
- (b) a reactant gas inlet defining a path of a molecular stream, where the reactant gas inlet is connected to a source of vanadium precursor, an oxidizing agent and a laser absorbing gas;
- (c) a laser beam path intersecting the path of the molecular stream; and
- (d) a product outlet.

The reactant gas inlet preferably is elongated in one dimension. The apparatus can further include a  $\text{CO}_2$ ,

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laser aligned to produce a laser beam along the laser beam path.

In another aspect, the invention features a process for converting nanoparticles of vanadium oxide 5 to other forms of vanadium oxide comprising the step of heating the nanoparticles of vanadium oxide in an oxidizing or inert atmosphere at a temperature at least about 300°C below the melting point of both the nanoparticles of vanadium oxide particles and the other 10 forms of vanadium oxide. The temperature preferably is between about 60°C and about 800 °C and more preferably between about 60°C and about 500°C.

The heating can be performed in an oxidizing atmosphere, which can include O<sub>2</sub>, O<sub>3</sub>, CO, CO<sub>2</sub>, or 15 combinations thereof. The oxidizing atmosphere can include between about 1 percent oxidizing gas and about 99 percent oxidizing gas by partial pressure. The oxidizing atmosphere can include flowing gas. The nanoparticles of vanadium oxide can include VO<sub>1.27</sub>, VO<sub>2</sub>, 20 V<sub>2</sub>O<sub>3</sub>, V<sub>3</sub>O<sub>5</sub>, amorphous V<sub>2</sub>O<sub>5</sub>, or 2-D crystalline V<sub>2</sub>O<sub>5</sub>. The other forms of vanadium oxide can include 2-D crystalline V<sub>2</sub>O<sub>5</sub> or crystalline V<sub>2</sub>O<sub>5</sub>. The nanoparticles 25 of vanadium oxide preferably have an average diameter from about 5 nm to about 500 nm or more preferably from about 5 nm to about 150 nm.

In another aspect, the invention features vanadium oxide nanoparticles formed by heating in an oxidizing or inert atmosphere, vanadium oxide nanoparticles of a different form. The vanadium oxide 30 nanoparticles of a different form preferably have an average diameter from about 5 nm to about 150 nm. In some embodiments, the vanadium oxide nanoparticles formed by heating have a higher oxygen to vanadium ratio than the vanadium oxide nanoparticles of a different

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form. The vanadium oxide particles formed by heating can include  $V_2O_5$ .

In another aspect, the invention features a process for forming vanadium oxide particles including 5 the step of heating particles of vanadium oxide with a lower oxygen to vanadium ratio than the vanadium oxide particles to be formed, in an oxidizing atmosphere at a temperature at least about 300°C below the melting point of both the vanadium oxide particles to be heated and 10 the vanadium oxide particles to be formed. The temperature preferably is between about 60°C and about 800°C, and more preferably between about 80°C and about 500°C.

The oxidizing atmosphere can comprise  $O_2$ ,  $O_3$ , 15  $CO$ ,  $CO_2$  or combinations thereof. The oxidizing atmosphere can include from about 1 percent oxidizing gas and 99 percent oxidizing gas by partial pressure. The initial vanadium oxide particles preferably have an average diameter from about 5 nm to about 1000 nm, and 20 more preferably from about 5 nm to about 150 nm. The product vanadium oxide particles can comprise orthorhombic  $V_2O_5$  crystals or 2-D  $V_2O_5$  crystals.

In another aspect, the invention features a process for forming crystalline  $V_2O_5$  including the step 25 of heating amorphous  $V_2O_5$  at a temperature at least about 300°C below the melting point of both the amorphous  $V_2O_5$  and the crystalline  $V_2O_5$ . The temperature preferably is between about 60°C and about 800°C. The amorphous  $V_2O_5$  particles preferably have an average 30 diameter from about 5 nm to about 1000 nm.

In another aspect, this invention features a cathode composition including vanadium oxide particles having an average diameter less than about 1000 nm and a binder. The vanadium oxide particles preferably have

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an average diameter from about 5 nm to about 150 nm and more preferably from about 5 nm to about 50 nm. The binder can be polyvinylidene fluoride, polyethylene oxide, polyethylene, polypropylene, 5 polytetrafluoroethylene, polyacrylates, mixtures thereof or copolymers thereof. The cathode composition can further include supplementary electrically conductive particles. The supplementary electrically conductive particles can include carbon. The cathode composition 10 preferably includes from about 60 percent by weight to about 98 percent by weight vanadium oxide particles.

In another aspect, the invention features a battery including an anode, a cathode comprising vanadium oxide particles having an average diameter less than about 1000 nm and a binder, and a separator element disposed between the anode and cathode. The anode can include lithium metal or a composition that intercalates lithium. Suitable intercalation compounds for the anode include, for example, carbon compounds. The vanadium 15 oxide particles preferably have an average diameter from about 150 nm to about 5 nm. The separator element can include a polymer electrolyte or a porous polymeric material. 20

In another aspect, the invention features a battery including an anode, an electrolyte, a cathode 25 and a separator element disposed between the anode and the cathode, the electrolyte comprising lithium ions and the cathode comprising nanoparticles of intercalation type, electroactive material and a binder, wherein the electroactive material in the cathode performs with an 30 energy density greater than about 900 Wh/kg during discharge of the battery. The battery can be a secondary battery. The electroactive material of the cathode can have an energy density from about 950 Wh/kg

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to about 1200 Wh/kg. The electroactive material can include vanadium oxide. The electroactive material in the anode can include a lithium intercalation composition.

5       The present invention involves vanadium oxide nanoparticles that possess enhanced properties for selected applications due to the very small particle size and correspondingly large surface area. Vanadium oxide nanoparticles have been produced with a variety of  
10      oxidation states and crystal structures. The particles generally have a narrow distribution of particle diameters. The particles can be produced using laser pyrolysis alone or combined with additional heating possibly in the presence of an oxidizing atmosphere.  
15      Laser pyrolysis is a very versatile technique as applied herein for producing a variety of vanadium oxide nanoparticles, which can be subjected to further processing, if desired.

20      In addition, the heat based processes described herein provide valuable pathways to producing important vanadium oxide materials. The processes are efficient and low cost. The techniques are particularly valuable for producing nanoparticles. Vanadium oxide nanoparticles produced using the heat based processes  
25      exhibit improved properties when incorporated into cathodes for lithium based batteries.

30      Batteries based on nanoparticles such as vanadium oxide nanoparticles lead to lithium batteries and lithium ion batteries with improved performance characteristics. In particular, the vanadium oxide nanoparticles have increased energy densities compared with larger diameter vanadium oxide particles. Using electroactive materials with increased energy densities yields batteries with higher capacities for a given

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amount of electroactive material. In this way, longer lasting, lighter and/or smaller batteries can be produced.

5 Other features and advantages of the invention will be apparent from the following description of the preferred embodiments, and from the claims.

BRIEF DESCRIPTION OF THE DRAWINGS

10 Fig. 1 is a schematic illustration of the effect on surface area of a reduction in particle diameter.

15 Fig. 2 is a schematic, sectional view of an embodiment of a laser pyrolysis apparatus taken through the middle of the laser radiation path. The upper insert is a bottom view of the injection nozzle, and the lower insert is a top view of the collection nozzle.

20 Fig. 3 is a schematic, perspective view of a reaction chamber of an alternative embodiment of the laser pyrolysis apparatus, where the materials of the chamber are depicted as transparent to reveal the interior of the apparatus.

Fig. 4 is a sectional view of the reaction chamber of Fig. 3 taken along line 4-4.

25 Fig. 5 is a schematic, sectional view of an oven for heating vanadium oxide particles, in which the section is taken through the center of the quartz tube.

Fig. 6 is a schematic, perspective view of a battery of the invention.

30 Fig. 7 is a schematic, perspective view of the three electrode arrangement used in the examples.

Fig. 8 is an x-ray diffractogram of amorphous  $V_2O_5$  nanoparticles.

Fig. 9 is an x-ray diffractogram of 2-D crystals of  $V_2O_5$  nanoparticles.

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Fig. 10 is a transmission electron microscope view of amorphous V<sub>2</sub>O<sub>5</sub> nanoparticles.

Fig. 11 is an x-ray diffractogram of crystalline VO<sub>2</sub> nanoparticles.

5 Fig. 12 is a transmission electron microscope view of crystalline VO<sub>2</sub> nanoparticles at lower magnification.

10 Fig. 13 is a transmission electron microscope view of crystalline VO<sub>2</sub> nanoparticles at higher magnification.

Fig. 14 is a plot depicting the distribution of particle sizes for the crystalline VO<sub>2</sub> nanoparticles depicted in Figs. 10 and 11.

15 Fig. 15 is an x-ray diffractogram of crystalline VO<sub>1.27</sub> nanoparticles.

Fig. 16 is an x-ray diffractogram of V<sub>6</sub>O<sub>13</sub> / VO<sub>2</sub> mixed phase nanoparticles.

Fig. 17 is an x-ray diffractogram of VO<sub>2</sub>/V<sub>2</sub>O<sub>3</sub> mixed phase nanoparticles.

20 Fig. 18 is an x-ray diffractogram of single phase crystalline V<sub>2</sub>O<sub>5</sub> nanoparticles.

Fig. 19 is an x-ray diffractogram of single phase crystalline V<sub>2</sub>O<sub>5</sub> nanoparticles produced using different starting materials than used to produce the 25 particles which generated the diffractogram in Fig. 18.

Fig. 20 is an x-ray diffractogram of crystalline V<sub>2</sub>O<sub>5</sub> nanoparticles made from VO<sub>2</sub> nanoparticles.

30 Fig. 21 is an x-ray diffractogram of VO<sub>2</sub> nanoparticles.

Fig. 22 is an x-ray diffractogram of crystalline V<sub>2</sub>O<sub>5</sub> nanoparticles made with a flow rate of O<sub>2</sub> of 4.8 sccm.

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Fig. 23 is an x-ray diffractogram of crystalline V<sub>2</sub>O<sub>5</sub> nanoparticles made with a flow rate of O<sub>2</sub> of 10.1 sccm.

5 Fig. 24 is an x-ray diffractogram of crystalline V<sub>2</sub>O<sub>5</sub> nanoparticles made with a flow rate of O<sub>2</sub> of 20.9 sccm.

Fig. 25 is an x-ray diffractogram of mixed phase 2-D crystalline V<sub>2</sub>O<sub>5</sub>/VO<sub>2</sub> made from VO<sub>2</sub> nanoparticles.

10 Fig. 26 is an x-ray diffractogram of 2-D crystalline V<sub>2</sub>O<sub>5</sub> made from amorphous V<sub>2</sub>O<sub>5</sub>.

Fig. 27 depicts the discharge/recharge cycling of a battery of the invention using VO<sub>2</sub> electroactive particles.

15 DETAILED DESCRIPTION OF THE PREFERRED EMBODIMENTS

Vanadium oxide particles having diameters substantially less than a micron have been produced. Vanadium oxides nanoparticles have been made in a variety of oxidation states and with a variety of 20 lattice structures. In particular, single phase crystalline nanoparticles have been demonstrated along with mixed phase nanoparticles and single phase amorphous nanoparticles.

25 To generate the desired nanoparticles, laser pyrolysis is used either alone or in combination with additional processing. Specifically, laser pyrolysis has been found to be a powerful technique for producing a variety of vanadium oxides nanoparticles. In addition, nanoscale vanadium oxide particles produced by 30 laser pyrolysis can be subjected to heating in an oxygen environment or an inert environment to alter the properties (type) of vanadium oxide without destroying the nanoparticle size. These nanoscale vanadium oxide particles from laser pyrolysis provide useful starting

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material for further processing with heat. Therefore, the combination of laser pyrolysis along with heat processing provides the means to produce many forms of vanadium oxide nanoparticles, with alternative routes of production being available for, at least, some of the vanadium oxide nanoparticles.

The small size of the particles results in a significantly increased surface area for a given weight of material. The increased surface area is depicted graphically in Fig. 1., assuming spherical particles and no aggregation.

The increased surface area of the nanoparticles can be advantageous for certain application. For example, cathodes for lithium based batteries incorporating the vanadium oxide nanoparticles exemplify improved performance, in particular, very high energy densities.

The vanadium oxide nanoparticles not only have high surface area resulting from their small size, but they also can have a high degree of crystallinity. This high degree of crystallinity generally is maintained throughout each nanoparticle. Nanocrystalline materials generally do not rely on pores to generate a high surface area. Pores can be undesirable since they represent a discontinuity in the crystalline lattice. The surface area of the nanoparticles generally results only from the faces of the particle.

A basic feature of successful application of laser pyrolysis for the production of vanadium oxide nanoparticles is production of a molecular stream containing a vanadium precursor, a radiation absorber and an oxygen source. The molecular stream is pyrolyzed by an intense laser beam. The intense heat resulting from the absorption of the laser radiation induces the

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oxidation of the vanadium precursor in the oxidizing environment. The laser pyrolysis provides for formation of phases of vanadium oxide that are difficult to form under thermodynamic equilibrium conditions. As the  
5 molecular stream leaves the laser beam, the vanadium oxide particles are rapidly quenched.

A route for producing a variety of desirable vanadium oxide particles involves heating particles of an initial type of vanadium oxide to convert them to the  
10 product particles. The heating step generally is performed in an oxidizing atmosphere, although for certain starting materials and corresponding products, an inert atmosphere generally is sufficient. Using these processing techniques, vanadium oxide particles  
15 can be formed with a higher relative oxygen content and/or with a different crystal lattice relative to the starting material. The conversion results from heating at surprisingly low temperatures well below the melting point of the materials. With mild processing  
20 temperatures, the particles generally do not significantly sinter.

These processes are especially desirable for the processing of nanoscale particles, i.e., particles having a diameter below a micron. Since the particles  
25 do not significantly sinter, the nanoscale of the particles is preserved during the heat processing. Alternatively, the particles can be heated to slightly higher temperatures to sinter the particles in a controlled fashion to form somewhat larger particles, as  
30 desired.

The vanadium oxide nanoparticles can be incorporated into a cathode film with a polymeric binder. The resulting film is appropriate for use as a cathode. While some of the vanadium oxides are

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reasonable electrical conductors, the film preferably incorporates additional electrically conductive particles held by the binder along with the vanadium oxide particles. The cathode film can be used in a  
5 lithium battery or a lithium ion battery.

Appropriate vanadium oxide nanoparticles incorporated into a cathode for a lithium based battery exhibit a significantly increased energy density relative to comparable materials of larger particle  
10 size. Amorphous nanoparticles can also be produced. Amorphous vanadium oxides can have very high energy densities. Amorphous bulk particles, however, can undergo crystalline rearrangements that reduce the energy density during the cycling of secondary  
15 batteries.

Vanadium oxide nanoparticles produced by heat processing have been found to be especially useful for the production of lithium based batteries. In particular, when used as a cathode active material, the  
20 vanadium oxide nanoparticles produced by heat processing have been found to yield very high energy densities. Crystalline V<sub>2</sub>O<sub>5</sub> nanoparticles have an energy density for lithium based battery applications several times the theoretical maximum energy density values of  
25 corresponding bulk (i.e., greater than micron sized) particles.

A. Particle Production

Laser pyrolysis has been discovered to be a valuable tool for the production of nanoscale vanadium oxide particles. In addition, the vanadium oxide nanoparticles produced by laser pyrolysis are a convenient material for further processing to expand the pathways for the production of certain vanadium oxide nanoparticles. Thus, using laser pyrolysis alone or in  
30

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combination with additional processes, a wide variety of vanadium oxide nanoparticles can be produced. In some cases, alternative production pathways can be followed to produce comparable particles.

5       The reaction conditions determine the qualities of the vanadium oxide particles produced by laser pyrolysis. The appropriate reaction conditions to produce a certain type of nanoparticles generally depend on the design of the particular apparatus. The reaction  
10      conditions for laser pyrolysis can be controlled relatively precisely in order to produce nanoparticles with desired properties. Specific conditions used to produce a variety of nanoparticles in a particular apparatus are described below in the examples.  
15      Nevertheless, some general observations on the relationship between reaction conditions and the resulting nanoparticles can be made.

20      Increasing the laser power results in increased reaction temperatures in the reaction region as well as a faster quenching rate. A rapid quenching rate tends to favor production of  $\text{VO}_2$ . Similarly, increasing the chamber pressure also tends to favor the production of higher energy structures, such as  $\text{VO}_2$ .  
25      Also, increasing the concentration of oxygen source in the reactant stream favors the production of vanadium oxides with increased amounts of oxygen, i.e., higher oxidation states of vanadium.

30      Reactant gas flow rate and velocity of the reactant gas stream are inversely related to particle size so that increasing the reactant gas flow rate or velocity tends to result in smaller particle size. Also, the growth dynamics of the particles have a significant influence on the size of the resulting particles. In other words, different crystal forms of

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vanadium oxide have a tendency to form different size particles from other crystal forms under relatively similar conditions. Laser power also influences particle size with increased laser power favoring larger  
5 particle formation for lower melting materials and smaller particle formation for higher melting materials.

Appropriate precursor compounds generally include vanadium compounds with reasonable vapor pressures, i.e., vapor pressures sufficient to get  
10 desired amounts of precursor vapor in the reactant stream. The vessel holding the precursor compounds can be heated to increase the vapor pressure of the vanadium precursor, if desired. Suitable vanadium precursors include, for example, VCl<sub>3</sub>, VCl<sub>4</sub>, VCCl<sub>3</sub>, V(CO)<sub>6</sub> and VOCl<sub>3</sub>.  
15 The Cl in these representative precursor compounds can be replaced with other halogens, e.g., Br, I and F. Preferred oxygen sources include, for example, O<sub>2</sub>, CO,  
CO<sub>2</sub>, O<sub>3</sub> and mixtures thereof. The oxygen source should not react significantly with the vanadium precursor  
20 prior to entering the reaction zone since this generally would result in the formation of large particles.

Laser pyrolysis can be performed with a variety of optical laser frequencies. Preferred lasers operate in the infrared portion of the electromagnetic  
25 spectrum. CO<sub>2</sub> lasers are particularly preferred sources of laser light. Infrared absorbers for inclusion in the molecular stream include, for example, C<sub>2</sub>H<sub>4</sub>, NH<sub>3</sub>, SF<sub>6</sub> and O<sub>3</sub>. O<sub>3</sub> can act as both an infrared absorber and as an oxygen source. The radiation absorber, such as the  
30 infrared absorber, absorbs energy from the radiation beam and distributes the energy as heat to the other reactants to drive the pyrolysis.

Preferably, the energy absorbed from the radiation beam increases the temperature at a tremendous

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rate, many times the rate that energy generally would be produced even by strongly exothermic reactions under controlled condition. While the process generally involves nonequilibrium conditions, the temperature can 5 be described approximately based on the energy in the absorbing region. The laser pyrolysis process is qualitatively different from the process in a combustion reactor where an energy source initiates a reaction, but the reaction is driven by energy given off by an 10 exothermic reaction.

An inert shielding gas can be used to reduce the amount of reactant and product molecules contacting the reactant chamber components. For the production of vanadium oxide nanoparticles, appropriate shielding 15 gases include, for example, Ar, He and N<sub>2</sub>.

An appropriate laser pyrolysis apparatus generally includes a reaction chamber isolated from the ambient environment. A reactant inlet connected to a reactant supply system produces a molecular stream through the reaction chamber. A laser beam path intersects the molecular stream at a reaction zone. The molecular stream continues after the reaction zone to an outlet, where the molecular stream exits the reaction chamber and passes into a collection system. Generally, 20 the laser is located external to the reaction chamber, and the laser beam enters the reaction chamber through 25 an appropriate window.

Referring to Fig. 2, a particular embodiment 100 of a pyrolysis apparatus involves a reactant supply 30 system 102, reaction chamber 104, collection system 106 and laser 108. Reactant supply system 102 includes a source 120 of vanadium precursor. For liquid precursors, a carrier gas from carrier gas source 122 can be introduced into precursor source 120, containing

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liquid precursor to facilitate delivery of the precursor. The carrier gas from source 122 preferably is either an infrared absorber or an inert gas and is preferably bubbled through the liquid vanadium 5 precursor. The quantity of precursor vapor in the reaction zone is roughly proportional to the flow rate of the carrier gas.

Alternatively, carrier gas can be supplied directly from infrared absorber source 124 or inert gas 10 source 126, as appropriate. The oxidizing agent is supplied from source 128, which can be a gas cylinder. The gases from the vanadium precursor source 120 are mixed with gases from oxidizing agent source 128, infrared absorber source 124 and inert gas source 126 by 15 combining the gases in a single portion of tubing 130. The gases are combined a sufficient distance from reaction chamber 104 such that the gases become well mixed prior to their entrance into reaction chamber 104. The combined gas in tube 130 passes through a duct 132 20 into rectangular channel 134, which forms part of an injection nozzle for directing reactants into the reaction chamber 104.

Flow from sources 122, 124, 126 and 128 are 25 preferably independently controlled by mass flow controllers 136. Mass flow controllers 136 preferably provide a controlled flow rate from each respective source. Suitable mass flow controllers include, for example, Edwards Mass Flow Controller, Model 825 series, from Edwards High Vacuum International, Wilmington, MA.

Inert gas source 138 is connected to an inert 30 gas duct 140, which flows into annular channel 142. A mass flow controller 144 regulates the flow of inert gas into inert gas duct 140. Inert gas source 126 can also

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function as the inert gas source for duct 140, if desired.

The reaction chamber 104 includes a main chamber 200. Reactant supply system 102 connects to the main chamber 200 at injection nozzle 202. The end of injection nozzle 202 has an annular opening 204 for the passage of inert shielding gas, and a rectangular slit 206 for the passage of reactant gases to form a molecular stream in the reaction chamber. Annular opening 204 has, for example, a diameter of about 1.5 inches and a width along the radial direction of about 1/16 in. The flow of shielding gas through annular opening 204 helps to prevent the spread of the reactant gases and product particles throughout reaction chamber 104.

Tubular sections 208, 210 are located on either side of injection nozzle 202. Tubular sections 208, 210 include ZnSe windows 212, 214, respectively. Windows 212, 214 are about 1 inch in diameter. Windows 212, 214 are preferably plano-focusing lenses with a focal length equal to the distance between the center of the chamber to the surface of the lens to focus the beam to a point just below the center of the nozzle opening. Windows 212, 214 preferably have an antireflective coating. Appropriate ZnSe lenses are available from Janos Technology, Townshend, Vermont. Tubular sections 208, 210 provide for the displacement of windows 212, 214 away from main chamber 200 such that windows 212, 214 are less likely to be contaminated by reactants or products. Window 212, 214 are displaced, for example, about 3 cm from the edge of the main chamber 200.

Windows 212, 214 are sealed with a rubber o-ring to tubular sections 208, 210 to prevent the flow of ambient air into reaction chamber 104. Tubular inlets

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216, 218 provide for the flow of shielding gas into tubular sections 208, 210 to reduce the contamination of windows 212, 214. Tubular inlets 216, 218 are connected to inert gas source 138 or to a separate inert gas 5 source. In either case, flow to inlets 216, 218 preferably is controlled by a mass flow controller 220.

Laser 108 is aligned to generate a laser beam 222 that enters window 212 and exits window 214. Windows 212, 214 define a laser light path through main 10 chamber 200 intersecting the flow of reactants at reaction zone 224. After exiting window 214, laser beam 222 strikes power meter 226, which also acts as a beam dump. An appropriate power meter is available from Coherent Inc., Santa Clara, CA. Laser 108 can be 15 replaced with an intense conventional light source such as an arc lamp. Preferably, laser 108 is an infrared laser, especially a CW CO<sub>2</sub> laser such as an 1800 watt maximum power output laser available from PRC Corp., Landing, NJ or a Coherent® model 525 (Coherent, Inc., 20 Santa Clara, CA) with a maximum power output of 375 watts.

Reactants passing through slit 206 in injection nozzle 202 initiate a molecular stream. The molecular stream passes through reaction zone 224, where 25 reaction involving the vanadium precursor takes place. Heating of the gases in reaction zone 224 is extremely rapid, roughly on the order of 10<sup>5</sup>°C/sec depending on the specific conditions. The reaction is rapidly quenched upon leaving reaction zone 224, and nanoparticles 228 are formed in the molecular stream. The nonequilibrium nature of the process allows for the 30 production of nanoparticles with a highly uniform size distribution and structural homogeneity.

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The path of the molecular stream continues to collection nozzle 230. Collection nozzle 230 is spaced about 2 cm from injection nozzle 202. The small spacing between injection nozzle 202 and collection nozzle 230 helps reduce the contamination of reaction chamber 104 with reactants and products. Collection nozzle 230 has a circular opening 232. Circular opening 232 feeds into collection system 106.

The chamber pressure is monitored with a pressure gauge attached to the main chamber. The chamber pressure generally ranges from about 5 Torr to about 1000 Torr. The preferred chamber pressure for the production of vanadium oxides ranges from about 80 Torr to about 300 Torr.

Reaction chamber 104 has two additional tubular sections not shown. One of the additional tubular sections projects into the plane of the sectional view in Fig. 2, and the second additional tubular section projects out of the plane of the sectional view in Fig. 2. When viewed from above, the four tubular sections are distributed roughly, symmetrically around the center of the chamber. These additional tubular sections have windows for observing the inside of the chamber. In this configuration of the apparatus, the two additional tubular sections are not used to facilitate production of nanoparticles.

Collection system 106 can include a curved channel 250 leading from collection nozzle 230. Because of the buoyant nature of the nanoparticles, the product nanoparticles follow the flow of the gas around curves. Collection system 106 includes a filter 252 within the gas flow to collect the product nanoparticles. A variety of materials such as teflon, glass fibers and the like can be used for the filter as long as the

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material is inert and has a fine enough mesh to trap the particles. Preferred materials for the filter include, for example, a glass fiber filter from ACE Glass Inc., Vineland, NJ.

5           Pump 254 is used to maintain collection system 106 at a reduced pressure. A variety of different pumps can be used. Appropriate pumps 254 include, for example, Busch Model B0024 pump from Busch, Inc., Virginia Beach, VA with a pumping capacity of about 25  
10 cubic feet per minute (cfm) and Leybold Model SV300 pump from Leybold Vacuum Products, Export, PA with a pumping capacity of about 195 cfm. It may be desirable to flow the exhaust of the pump through a scrubber 256 to remove any remaining reactive chemicals before venting into the  
15 atmosphere. The entire apparatus 100 can be placed in a fume hood for ventilation purposes and for safety considerations. Generally, the laser remains outside of the fume hood because of its large size.

The apparatus is controlled by a computer.  
20 Generally, the computer controls the laser and monitors the pressure in the reaction chamber. The computer can be used to control the flow of reactants and/or the shielding gas. The pumping rate is controlled by either a manual needle valve or an automatic throttle valve  
25 inserted between pump 254 and filter 252. As the chamber pressure increases due to the accumulation of particles on filter 252, the manual valve or the throttle valve can be adjusted to maintain the pumping rate and the corresponding chamber pressure.

30           The reaction can be continued until sufficient nanoparticles are collected on filter 252 such that the pump can no longer maintain the desired pressure in the reaction chamber 104 against the resistance through filter 252. When the pressure in reaction chamber 104

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can no longer be maintained at the desired value, the reaction is stopped, and the filter 252 is removed. With this embodiment, about 3-5 grams of nanoparticles can be collected in a single run before the chamber pressure can no longer be maintained. A single run generally can last from about 10 minutes to about 1 hour depending on the type of particle being produced and the particular filter. Therefore, it is straightforward to produce a macroscopic quantity of nanoparticles, i.e., 5 a quantity visible with the naked eye.

10

The reaction conditions can be controlled relatively precisely. The mass flow controllers are quite accurate. The laser generally has about 0.5 percent power stability. With either a manual control 15 or a throttle valve, the chamber pressure can be controlled to within about 1 percent.

The configuration of the reactant supply system 102 and the collection system 106 can be reversed. In this alternative configuration, the reactants are supplied from the bottom of the reaction 20 chamber, and the product particles are collected from the top of the chamber. This alternative configuration tends to result in a slightly higher collection of product since vanadium oxide nanoparticles tend to be buoyant in the surrounding gases. In this 25 configuration, it is preferable to include a curved section in the collection system so that the collection filter is not mounted directly above the reaction chamber.

30 An alternative design of a laser pyrolysis apparatus has been described. See, commonly assigned U.S. Patent Application No. 08/808,850, entitled "Efficient Production of Particles by Chemical Reaction," incorporated herein by reference. This

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alternative design is intended to facilitate production of commercial quantities of nanoparticles. A variety of configurations are described for injecting the reactant materials into the reaction chamber.

5       The alternative apparatus includes a reaction chamber designed to minimize contamination of the walls of the chamber with particles, to increase the production capacity and to make efficient use of resources. To accomplish these objectives, the reaction  
10      chamber conforms generally to the shape of an elongated reactant inlet, decreasing the dead volume outside of the molecular stream. Gases can accumulate in the dead volume, increasing the amount of wasted radiation through scattering or absorption by nonreacting  
15      molecules. Also, due to reduced gas flow in the dead volume, particles can accumulate in the dead volume causing chamber contamination.

20      The design of the improved reaction chamber 300 is schematically shown in Figs. 3 and 4. A reactant gas channel 302 is located within block 304. Facets 306 of block 304 form a portion of conduits 308. Another portion of conduits 308 join at edge 310 with an inner surface of main chamber 312. Conduits 308 terminate at shielding gas inlets 314. Block 304 can be repositioned  
25      or replaced, depending on the reaction and desired conditions, to vary the relationship between the elongated reactant inlet 316 and shielding gas inlets 314. The shielding gases from shielding gas inlets 314 form blankets around the molecular stream originating  
30      from reactant inlet 316.

      The dimensions of elongated reactant inlet 316 preferably are designed for high efficiency particle production. Reasonable dimensions for the reactant inlet for the production of vanadium oxide nanoparticle,

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when used with a 1800 watt CO<sub>2</sub> laser, are from about 5 mm to about 1 meter.

Main chamber 312 conforms generally to the shape of elongated reactant inlet 316. Main chamber 312 includes an outlet 318 along the molecular stream for removal of particulate products, any unreacted gases and inert gases. Tubular sections 320, 322 extend from the main chamber 312. Tubular sections 320, 322 hold windows 324, 326 to define a laser beam path 328 through the reaction chamber 300. Tubular sections 320, 322 can include shielding gas inlets 330, 332 for the introduction of shielding gas into tubular sections 320, 322.

The improved apparatus includes a collection system to remove the nanoparticles from the molecular stream. The collection system can be designed to collect a large quantity of particles without terminating production or, preferably, to run in continuous production by switching between different particle collectors within the collection system. The collection system can include curved components within the flow path similar to curved portion of the collection system shown in Fig. 2. The configuration of the reactant injection components and the collection system can be reversed such that the particles are collected at the top of the apparatus.

As noted above, properties of the vanadium oxide particles can be modified by further processing. The starting material for the heat treatment can be any type of solid vanadium oxide compound. Suitable materials include, for example, VO, VO<sub>1.27</sub>, VO<sub>2</sub>, V<sub>2</sub>O<sub>3</sub>, V<sub>3</sub>O<sub>5</sub> and amorphous V<sub>2</sub>O<sub>5</sub>. The starting materials generally can be particles of any size and shape. In addition, particles used as starting material can have been

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subjected to one or more prior heating steps under different conditions.

Nanoscale particles are preferred starting materials. The nanoscale particles have an average 5 diameter of less than about 1000 nm and preferably from about 500 nm to about 5 nm, and more preferably from about 150 nm to about 5 nm. Suitable nanoscale starting materials have been produced by laser pyrolysis. The heat processing can be performed on initial particles 10 that were not produced by laser pyrolysis, including particles that do not have a generally spherical shape, i.e., particles that are flat sheets or needle like.

The vanadium oxide particles are preferably heated in an oven or the like to provide generally 15 uniform heating. The processing conditions generally are mild. The temperature of heating is low relative to the melting point of both the starting material and the product material. The temperature generally is at least 300°C below the melting point and preferably at least 20 450°C below the melting point of either the starting material or the product material. For nanoparticles, the processing temperature generally ranges from about 50°C to about 500°C, and more preferably from about 60°C to about 400°C. For bulk particles, the temperature 25 ranges from about 80°C to about 1000°C and more preferably from about 100°C to about 800°C.

The heating preferably is continued for more than about 1 hour, and generally is continued for from 30 about 2 hours to about 100 hours, preferably from about 10 hours to about 50 hours. For certain target product particles, additional heating does not lead to further variation in the particle composition. The atmosphere for the heating process generally is an oxidizing atmosphere. For conversion of amorphous particles to

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crystalline particles or from one crystalline structure to a different crystalline structure of essentially the same stoichiometry, the atmosphere generally can be inert. The atmosphere over the particles can be static,  
5 or gases can be flowed through the system.

Appropriate oxidizing gases include, for example, O<sub>2</sub>, O<sub>3</sub>, CO, CO<sub>2</sub>, and combinations thereof. Oxidizing gases optionally can be mixed with inert gases such as Ar, He and N<sub>2</sub>. When inert gas is mixed with the  
10 oxidizing gas, the gas mixture can be from about 1 percent oxidizing gas to about 99 percent oxidizing gas, and more preferably from about 5 percent oxidizing gas to about 99 percent oxidizing gas. Alternatively,  
15 either essentially pure oxidizing gas or pure inert gas can be used, as desired.

The precise conditions can be altered to vary the type of vanadium oxide product produced. For example, the temperature, time of heating, heating and cooling rates, the gases and the exposure conditions  
20 with respect to the gases can all be changed, as desired. Generally, while heating under an oxidizing atmosphere, the longer the heating period the more oxygen that is incorporated into the material, prior to reaching equilibrium. Once equilibrium conditions are  
25 reached, the overall conditions determine the crystalline phase of the powders.

A variety of ovens can be used to perform the heating. An example of an apparatus 400 to perform this processing is displayed in Fig. 5. Apparatus 400 includes a tube 402 into which the particles are placed.  
30 Tube 402 generally is connected to an oxidizing gas source 404 and inert gas source 406. Oxidizing gas, inert gas or a combination thereof to produce the

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desired atmosphere are placed within tube 402 from the appropriate gas source(s).

Preferably, the desired gases are flowed through tube 402. Various flow rates can be used. The 5 flow rate preferably is between about 1 standard cubic centimeters per minute (sccm) to about 1000 sccm and more preferably from about 10 sccm to about 500 sccm. The flow rate generally is constant through the processing step, although the flow rate and the 10 composition of the gas can be varied systematically over time during processing, if desired. Alternatively, a static gas atmosphere can be used.

Tube 402 is located within oven or furnace 408. Oven 408 can be adapted from a commercial furnace 15 such as Mini-Mite™ 1100°C Tube Furnace from Revco/Lindberg, Asheville, NC. Oven 408 maintains the relevant portions of the tube at a relatively constant temperature, although the temperature can be varied systematically through the processing step, if desired. 20 Temperature in oven 408 generally is measured with a thermocouple 410.

The vanadium oxide particles can be placed in tube 402 within a vial 412. Vial 412 prevents loss of the particles due to gas flow. Vial 412 generally is 25 oriented with the open end directed toward the direction of the source of the gas flow. Alternatively, the particles could be placed within a material that would permit gas flow while holding the particles in place. For example, the collection filter from the laser 30 pyrolysis could be placed within the tube in an orientation that would tend to keep the particles on the filter material.

The precise conditions including the type of oxidizing gas (if any), concentration of oxidizing gas,

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pressure or flow rate of gas, temperature and processing time can be selected to produce the desired type of product material.

High melting point  $\text{VO}_2$  is relatively easy to form in the laser pyrolysis apparatuses described above.  $\text{VO}_2$  is a suitable starting product for oxidation to other forms of vanadium oxide. Some empirical adjustment may be required to produce the conditions appropriate to generate a desired material.

10 B. Properties of Vanadium Oxide Particles

Vanadium oxide has an intricate phase diagram due to the many possible oxidation states of vanadium. Vanadium is known to exist in oxidation states between  $\text{V}^{+5}$  and  $\text{V}^{+2}$ . The energy differences between the oxides of vanadium in the different oxidation states is not large. Therefore, it is possible to produce stoichiometric mixed valence compounds. Known forms of vanadium oxide include  $\text{VO}$ ,  $\text{VO}_{1.27}$ ,  $\text{V}_2\text{O}_3$ ,  $\text{V}_3\text{O}_5$ ,  $\text{VO}_2$ ,  $\text{V}_6\text{O}_{13}$ ,  $\text{V}_4\text{O}_9$ ,  $\text{V}_3\text{O}_7$ , and  $\text{V}_2\text{O}_5$ . The present processing approaches successfully yield single phase vanadium oxide in many different oxidation states, as evidenced by x-ray diffraction studies. These single phase materials are generally crystalline, although some amorphous nanoparticles have been produced. The present heat treatment approach is useful for increasing the oxidation state of vanadium oxide particles or for converting vanadium oxide particles to more ordered phases.

There are also mixed phase regions of the vanadium oxide phase diagram. In the mixed phase regions, particles can be formed that have domains with different oxidation states, or different particles can be simultaneously formed with vanadium in different oxidation states. In other words, certain particles or

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portions of particles have one stoichiometry while other particles or portions of particles have a different stoichiometry. Mixed phase nanoparticles have been formed as described below. Non-stoichiometric materials  
5 also can be formed.

The vanadium oxides generally form crystals with octahedral or distorted octahedral coordination. Specifically, VO, V<sub>2</sub>O<sub>3</sub>, VO<sub>2</sub>, V<sub>6</sub>O<sub>13</sub> and V<sub>3</sub>O<sub>8</sub> can form crystals with octahedral coordination. In addition,  
10 V<sub>3</sub>O<sub>8</sub> can form crystals with trigonal bipyramidal coordination. V<sub>2</sub>O<sub>5</sub> forms crystals with square pyramidal or distorted octahedral coordination. V<sub>2</sub>O<sub>5</sub> recently also has been produced in a two dimensional crystal structure. See, M. Hibino, et al., Solid State Ionics  
15 79:239-244 (1995), incorporated herein by reference. When produced under appropriate conditions, the vanadium oxide nanoparticles can be amorphous. The crystalline lattice of the vanadium oxide can be evaluated using x-ray diffraction measurements.

With heat processing, an increase in the oxidation state of vanadium within a vanadium oxide particles is generally accomplished within an oxidizing atmosphere. The conversion of a vanadium oxide to a more ordered crystalline lattice with the same  
25 stoichiometry generally can be accomplished with an oxidizing atmosphere or an inert atmosphere.

A collection of vanadium oxide nanoparticles has an average diameter of less than a micron, preferably from about 5 nm to about 500 nm and more preferably from about 5 nm to about 150 nm, and even more preferably from about 10 nm to about 50 nm. The nanoparticles generally have a roughly spherical gross appearance. Upon closer examination, the particles generally have facets corresponding to the underlying

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crystal lattice. Nevertheless, the nanoparticles tend to exhibit growth that is roughly equal in the three physical dimensions to give a gross spherical appearance. Diameter measurements on particles with  
5 asymmetries are based on an average of length measurements along the principle axes of the particle. The measurements along the principle axes preferably are each less than about 1 micron for at least about 95 percent of the nanoparticles, and more preferably for at  
10 least about 98 percent of the nanoparticles.

Because of their small size, the nanoparticles tend to form loose agglomerates due to van der Waals forces between nearby particles. Nevertheless, the nanometer scale of the particles is clearly observable  
15 in transmission electron micrographs of the particles. For crystalline nanoparticles, the particle size generally corresponds to the crystal size. The particles generally have a surface area corresponding to particles on a nanometer scale as observed in the  
20 micrographs. Furthermore, the particles manifest unique properties due to their small size and large surface area per weight of material, as described herein with respect to use of vanadium oxide nanoparticles in lithium based batteries.

25 The nanoparticles preferably have a high degree of uniformity in size. As determined from examination of transmission electron micrographs, the particles generally have a distribution in sizes such that at least about 95 percent of the particles have a diameter greater than about 40 percent of the average diameter and less than about 160 percent of the average diameter. Preferably, the nanoparticles have a distribution of diameters such that at least about 95 percent of the particles have a diameter greater than  
30

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about 60 percent of the average diameter and less than about 140 percent of the average diameter. In addition, the nanoparticles generally have a very high purity level. Vanadium oxide nanoparticles are expected to 5 have a purity greater than the reactant gases because the crystal formation process tends to exclude contaminants from the lattice.

The above described techniques have been successfully applied to the production of nanoparticles 10 of vanadium oxide with several different stoichiometries and with different crystal structures with the same stoichiometry. The structures and compositions have been examined using x-ray defractometry. The sizes of some of the particles have been examined using 15 transmission electron microscopy. The properties of the types of vanadium oxide nanoparticles obtained are summarized in Table 1.

Table 1

20

25

<u>Stoichiometry</u>	<u>Lattice</u>
Single Phase VO <sub>x</sub>	Monoclinic
Single Phase VO <sub>1-x</sub>	Tetragonal
Single Phase V <sub>2</sub> O <sub>5</sub>	Amorphous 2-D crystals Crystalline
Mixed Phase V <sub>x</sub> O <sub>1-x</sub> + VO <sub>x</sub>	V <sub>x</sub> O <sub>1-x</sub> , majority/Monoclinic
Mixed Phase V <sub>x</sub> O <sub>1-x</sub> + VO <sub>x</sub>	V <sub>x</sub> O <sub>1-x</sub> , majority/Rhombohedral

#### C. Lithium Based Batteries

Referring to Fig. 6, battery 450 has an anode 30 452, a cathode 454 and separator 456 between anode 452 and cathode 454. A single battery can include multiple cathodes and/or anodes. Electrolyte can be supplied in a variety of ways as described further below. Battery 450 preferably includes current collectors 458, 460

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associated with anode 452 and cathode 454, respectively. Multiple current collectors can be associated with each electrode if desired.

Lithium has been used in reduction/oxidation reactions in batteries because they are the lightest metal and because they are the most electropositive metal. Certain forms of vanadium oxide are known to incorporate lithium ions into its structure through intercalation or similar mechanisms such as topochemical absorption. Intercalation of lithium ions into suitable forms of a vanadium oxide lattice forms  $\text{Li}_x\text{VO}_y$ . Appropriate vanadium oxides can be an effective electroactive material for a cathode in either a lithium or lithium ion battery.

Lithium intercalated vanadium oxide is formed in the battery during discharge. The lithium leaves the lattice upon recharging, i.e., when a voltage is applied to the cell such that electric current flows into the cathode due to the application of an external EMF to the battery. Intercalation generally is reversible, making certain vanadium oxides suitable for the production of secondary batteries.

Cathode 454 includes electroactive nanoparticles such as vanadium oxide nanoparticles held together with a binder such as a polymeric binder. Nanoparticles for use in cathode 454 generally can have any shape, e.g., roughly spherical nanoparticles or elongated nanoparticles. Cathode 454 can include other electroactive nanoparticles such as  $\text{TiO}_2$  nanoparticles. The production of  $\text{TiO}_2$  nanoparticles has been described, see U.S. Patent Ser. No. 4,705,762, incorporated herein by reference.  $\text{TiO}_2$  nanoparticles are expected to exhibit relatively high energy densities in lithium

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based batteries by analogy with the results discovered for vanadium oxides nanoparticles.

While some of the electroactive materials, such as certain vanadium oxides, are reasonable electrical conductors, the cathode optionally can include electrically conductive particles in addition to the electroactive nanoparticles. These supplementary, electrically conductive particles generally are also held by the binder. Suitable electrically conductive particles include conductive carbon particles such as carbon black, metal particles such as silver particles and the like.

With vanadium oxide nanoparticles, very high energy densities have been achieved. Preferred vanadium oxide nanoparticles have energy densities in lithium based batteries significantly greater than the theoretical maximum values for the corresponding bulk vanadium oxide particles. Vanadium oxide nanoparticles preferably have energy densities at least about 150 percent of the theoretical maximum of the bulk material, and more preferably at least about 200 percent of the theoretical maximum of the bulk material. Specifically, preferred vanadium oxide nanoparticles in lithium based batteries have an energy density of at least about 900 Wh/kg, preferably at least about 1000 Wh/kg. Electroactive nanoparticles can have an energy density in the range from 1000 Wh/kg to about 1200 Wh/kg.

High loadings of particles can be achieved in the binder. Particles preferably make up greater than about 80 percent by weight of the cathode, and more preferably greater than about 90 percent by weight. The binder can be any of various suitable polymers such as polyvinylidene fluoride, polyethylene oxide,

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polyethylene, polypropylene, polytetrafluoroethylene, polyacrylates and mixtures and copolymers thereof.

Anode 452 can be constructed from a variety of materials that are suitable for use with lithium ion electrolytes. In the case of lithium batteries, the anode can include lithium metal or lithium alloy metal either in the form of a foil, grid or metal particles in a binder.

Lithium ion batteries use particles of an composition that can intercalate lithium. The particles are held with a binder in the anode. Suitable intercalation compounds include, for example, graphite, synthetic graphite, coke, mesocarbons, doped carbons, fullerenes, niobium pentoxide and  $\text{SnO}_2$ .

Current collectors 458, 460 facilitate flow of electricity from battery 450. Current collectors 458, 460 are electrically conductive and generally made of metal such as nickel, iron, stainless steel, aluminum and copper and can be metal foil or preferably a metal grid. Current collector 458, 460 can be on the surface of their associated electrode or embedded within their associated electrode.

The separator element 456 is electrically insulating and provides for passage of at least some types of ions. Ionic transmission through the separator provides for electrical neutrality in the different sections of the cell. The separator generally prevents electroactive compounds in the cathode from contacting electroactive compounds in the anode.

A variety of materials can be used for the separator. For example, the separator can be formed from glass fibers that form a porous matrix. Preferred separators are formed from polymers such as those suitable for use as binders. Polymer separators can be

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porous to provide for ionic conduction. Alternatively, polymer separators can be solid electrolytes formed from polymers such as polyethylene oxide. Solid electrolytes incorporate electrolyte into the polymer matrix to 5 provide for ionic conduction without the need for liquid solvent.

Electrolytes for lithium batteries or lithium ion batteries can include any of a variety of lithium salts. Preferred lithium salts have inert anions and 10 are nontoxic. Suitable lithium salts include, for example, lithium hexafluorophosphate, lithium hexafluoroarsenate, lithium bis(trifluoromethyl sulfonyl imide), lithium trifluoromethane sulfonate, lithium tris(trifluoromethyl sulfonyl) methide, lithium tetrafluoroborate, lithium perchlorate, lithium tetrachloroaluminate, lithium chloride and lithium perfluorobutane.

If a liquid solvent is used to dissolve the electrolyte, the solvent preferably is inert and does 20 not dissolve the electroactive materials. Generally appropriate solvents include, for example, propylene carbonate, dimethyl carbonate, diethyl carbonate, 2-methyl tetrahydrofuran, dioxolane, tetrahydrofuran, 1, 2-dimethoxyethane, ethylene carbonate,  $\gamma$ -butyrolactone, 25 dimethyl sulfoxide, acetonitrile, formamide, dimethylformamide and nitromethane.

The shape of the battery components can be adjusted to be suitable for the desired final product, for example, a coin battery, a rectangular construction 30 or a cylindrical battery. The battery generally includes a casing with appropriate portions in electrical contact with current collectors and/or electrodes of the battery. If a liquid electrolyte is used, the casing should prevent the leakage of the

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electrolyte. The casing can help to maintain the battery elements in close proximity to each other to reduce resistance within the battery. A plurality of battery cells can be placed in a single case with the  
5 cells connected either in series or in parallel.

#### Examples

These examples demonstrate the production of nanoscale vanadium oxides with various lattices and  
10 stoichiometry. The particles described in Examples 1-5 were produced using essentially the apparatus of Fig. 2 described above. The heat treatments described in the Examples were preformed in an oven essentially as described above with respect to Fig. 5. Between about  
15 100 and about 300 mg of nanoparticles were placed within an open 1 cc vial within the tube in the oven. The specific conditions for heat processing are described in the examples below.

In addition, vanadium oxide based lithium  
20 batteries were evaluated to determine the charge capacity and energy density of the vanadium oxide powders used as active materials in the cathodes. The batteries tested in the following examples were all produced following a common procedure. The vanadium  
25 oxide powders (VO) were mixed with a conductive acetylene black powder (AB) (Catalog number 55, Chevron Corp.) at a ratio of 60:30. The powder mixture was ground with a mortar and palette to thoroughly mix the powders.

30 A few drops of polyvinylidene fluoride (PVDF) solution were added to the homogeneous powder mixture. The 10 percent PVDF solution included PVDF (Catalog reference R-1, Elf Atochem North America, Inc., Philadelphia, PA) dissolved in 1-methyl-2-pyrrolidinone

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(Aldrich Chemical Co., Milwaukee, WI). The final ratio of VO:AB:PVDF was 60:30:10. The resulting slurry was spread onto a preweighed nickel metal mesh. The mesh with the slurry was baked in a vacuum oven overnight at 5 120°C to remove the solvent and residual moisture. After removal from the oven, the electrodes were immediately placed in a glove box (Vacuum Atmosphere Co., Hawthorne, CA) under an argon atmosphere and weighted again.

10 All discharge/charge experiments were conducted in the glove box. The water and oxygen concentrations in the glove box were measured to be less than 1 ppm and 1.5 ppm, respectively. The samples were tested in a three electrode configuration, as shown in 15 Fig. 7. In the test set up, cathode 502 on nickel mesh 504 is place in container 506. Container 506 holds liquid electrolyte 508. Counter electrode 510 and reference electrode 512 are also placed into container 506. Lithium metal was used as both counter electrode 20 and reference electrode. The electrodes are connected to a battery testing system 514.

No separator is needed for this testing configuration since the electrodes are physically separated. Alternatively, the liquid electrolyte can be 25 viewed as the separator. The liquid electrolyte (from Merck & Co., Inc.) was 1M LiClO<sub>4</sub> in propylene carbonate.

The samples were tested at the same discharge/charge rate of C/20 (i.e., a rate such that the cathode would be fully discharged in 20 hours), and 30 cycled between 4.0 volts and 1.8 volts at 25°C. The measurements were controlled by an Arbin Battery Testing System, Model BT4023, from Arbin Instruments, College Station, TX. The charging/discharging profiles were

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recorded, and the discharge capacity and energy density of the active materials were obtained.

The energy density is evaluated by the integral over the discharge time of the voltage multiplied by the current divided by the mass of the active material. The current is kept approximately constant during discharge. Currents used during testing ranged from about 0.08 mA to about 0.12 mA. The current is adjusted to have an approximately constant current density for all the tests. The current density was about 0.1 mA/cm<sup>2</sup>. The active material mass ranged from about 5 to about 17 mg.

Example 1 - Single phase V<sub>2</sub>O<sub>5</sub> - Laser Pyrolysis

The synthesis of V<sub>2</sub>O<sub>5</sub> described in this example was performed by laser pyrolysis. The VOCl<sub>3</sub> (Strem Chemical, Inc., Newburyport, MA) precursor vapor is carried into the reaction chamber by bubbling Ar gas through the VOCl<sub>3</sub> liquid stored in a container at room temperature. The reactant gas mixture containing VOCl<sub>3</sub>, Ar, O<sub>2</sub> and C<sub>2</sub>H<sub>4</sub> is introduced into the reactant gas nozzle for injection into the reactant chamber. The reactant gas nozzle had an opening with dimensions as specified in Table 2. C<sub>2</sub>H<sub>4</sub> gas acts as a laser absorbing gas. Argon was used as an inert gas.

The synthesized vanadium oxide nanoscale particles can be directly handled in the air. The production rate was typically about 5 - 10 g/hour of nanoparticles. The samples were subsequently examined by transmission electron microscopy (TEM) to determine particle sizes and by x-ray diffraction to evaluate the composition and structure.

Using laser pyrolysis, both amorphous V<sub>2</sub>O<sub>5</sub> and 2-D crystalline V<sub>2</sub>O<sub>5</sub> have been produced. Representative

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reaction conditions used to produce these particles are described in the following table.

TABLE 2

	V <sub>2</sub> O <sub>5</sub>			
Phase	Amorphous	Amorphous	Amorphous	2D Crystal
Crystal Structure				
Battery Capacity (mAh/g)	182			146
Pressure (Torr)	135	142.5	110	300
Argon - Win. (sccm)	700	700	700	700
Argon - Sld. (slm)	0.98	0.98	2.1	1.12
Ethylene (sccm)	603	1072	173	268
Carrier Gas (sccm)	116(Ar)	676(Ar)	140(Ar)	676(Ar)
Oxygen (sccm)	284	642	88	400
Laser Output (watts)	180	215	150	67
Nozzle Size	5/8" x 1/16"	5/8" x 1/16"	5/8" x 1/8"	5/8" x 1/16"

sccm = standard cubic centimeters per minute

slm = standard liters per minute

Argon - Win. = argon flow through inlets 216, 218

Argon - Sld. = argon flow through annular channel 142

Representative x-ray diffractograms for amorphous V<sub>2</sub>O<sub>5</sub> and 2-D V<sub>2</sub>O<sub>5</sub> are shown in Figs. 8 and 9, respectively. The x-ray diffractograms were obtained using Cu(Kα) radiation line on a Siemens D500 x-ray diffractometer. Referring to Fig. 8, the broad peaks centered around 2θ ~ 28 degrees and 58 degrees are typical of amorphous phase of vanadium oxide. See, U.S. Patent No. 4,675,260. The amorphous nature of the sample is confirmed by transmission electron microscopy examination as shown in Fig. 10. The TEM micrograph shows a material that has disordered atomic arrangement.

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The diffractogram in Fig. 9 corresponds to a recently reported 2-D crystal structure for  $V_2O_5$ . See, x-ray diffractogram in Fig. 2 of Hibino et al., above. The materials described by Hibino et al. had been made  
5 using liquid phase reactions.

Example 2 - Single Phase  $VO_2$

These particles were produced using a similar laser pyrolysis set up as described in Example 1. The reactant gas nozzle had dimensions 5/8 in x 1/16 in.  
10 For the production of  $VO_2$ ,  $C_2H_4$  was bubbled through the  $VOCl_3$  liquid precursor at room temperature. Representative reaction conditions for the production of this material are described in Table 3.

15

Table 3

Phase	$VO_2$	$VO_x$	$VO_{1.27}$
Crystal Structure	Monoclinic	Monoclinic	Tetragonal
Battery Capacity (mAh/g)	249		118.4
Pressure (Torr)	320	127	200
Argon-Win (sccm)	700	700	700
Argon-Sld. (slm)	5.6	0.98	2.8
Ethylene (sccm)	460	268	402
Carrier Gas (sccm)	460(Ethyl.)	676(Ar)	402(Ethyl.)
Oxygen (sccm)	36	200	196
Laser Output (watts)	96	220	100

30

An x-ray diffractogram of representative product nanoparticles is shown in Fig. 11. Clear diffraction peaks corresponding to a monoclinic crystalline structure are visible. The identified structure from the diffractogram is almost identical to that of the corresponding bulk material, which has  
35

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larger particle sizes. Therefore, the novel nanoparticle materials have distinct properties while maintaining the same crystalline lattice of the bulk material.

5 TEM photos at both high and low magnifications were obtained of representative nanoparticles with similar x-ray diffraction patterns, as shown in Figs. 12 and 13. An approximate size distribution was determined by manually measuring diameters of the particles shown  
10 in Fig. 12. The distribution of diameters is shown in Fig. 14. An average particle size of about 22 nm was obtained. Only those particles showing clear particle boundaries were measured and recorded to avoid regions of distorted in the micrograph. This should not bias  
15 the measurements obtained since the single view of the micrograph may not show a clear view of all particles because of the orientation of the crystals. It is significant that the particles span a rather narrow range of sizes. In this case, the largest to the  
20 smallest particles differ by no more than about 15 nm. Crystallinity of the particles is confirmed in Fig. 13 where the underlying lattice structure is visible.

Example 3 - Single Phase VO<sub>1.27</sub>,

25 The experimental arrangement for the production of VO<sub>1.27</sub> is the same as that described in Example 2. Representative conditions used to produce these particles are given in Table 3, above.

30 The x-ray diffractogram for this material is shown in Fig. 15, and is characteristic of crystalline VO<sub>1.27</sub> material.

Example 4 - V<sub>6</sub>O<sub>13</sub>/VO<sub>2</sub> Mixed Phase Material

The experimental configuration was the same as described with respect to Example 1. The reactant gas

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nozzle had dimensions 5/8 in x 1/8 in. The particular experimental parameters are given in Table 4.

Table 4

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Phase	$V_6O_{13}$ + $VO_2$	$V_6O_{13}$ + $VO_3$	$VO_2$ + $V_2O_3$
Crystal Structure	Monoclinic	Monoclinic	
Pressure (Torr)	110	110	410
Argon - Win (sccm)	700	700	700
Argon - Sld. (slm)	2.1	2.1	11.2
Ethylene (sccm)	173	209	460
Carrier Gas (sccm)	140 (Ar)	140 (Ar)	Ethylene
Oxygen (sccm)	88	88	36
Laser Output (watts)	192	100	90

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A characteristic x-ray diffractogram of the nanoparticles is shown in Fig. 16. The diffractogram contains a combination of peaks identifiable with both crystalline  $V_6O_{13}$  and crystalline  $VO_2$ . Both types of crystals are monoclinic. The  $V_6O_{13}$  phase is the majority phase. Appropriate reaction conditions should yield single phase  $V_6O_{13}$ .

#### Example 5 - $VO_2/V_2O_3$ Mixed Phase Material

The experimental configuration was the same as described with respect to Example 4. The reactant gas nozzle had dimensions 5/8 in x 1/16 in. Representative experimental parameters to produce these particles are given in Table 4, above. The x-ray diffractogram is shown in Fig. 17. The diffractogram contains a combination of peaks identifiable with both crystalline  $VO_2$  and crystalline  $V_2O_3$ . Note that the conditions for the production of these particles involves a reduced amount of  $O_2$  relative to the other gases in the reactant stream.

#### Example 6 - Crystalline $V_2O_5$ - Oven Processed

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A first sample of crystalline  $V_2O_5$  was produced from amorphous  $V_2O_5$  by baking the amorphous particles in an oven for 16.0 hours. The amorphous  $V_2O_5$  starting material was produced by laser pyrolysis 5 according to the parameters in the second column of Table 2. The oven was set at a temperature of 202°C. Oxygen gas flowed through a 1.0 in. diameter quartz tube at a flow rate of 105.6 sccm. Between about 100 and about 300 mg of nanoparticles were placed within an open 10 1 cc vial within the tube in the oven. The resulting nanoparticles were single phase crystalline  $V_2O_5$  nanoparticles. The corresponding x-ray diffractogram is presented in Fig. 18. The x-ray diffractogram is characteristic of orthorhombic  $V_2O_5$ .

15 A second sample of crystalline  $V_2O_5$  were made from crystalline  $VO_2$  using the same starting materials. The starting materials were crystalline  $VO_2$  nanoparticles produced by laser pyrolysis using the conditions specified in the second column of Table 3. 20 The second sample was treated in an oven under the same conditions as the first sample.

The resulting nanoparticles for the second sample were single phase  $V_2O_5$ . These had a smaller average diameter than the particles from the first 25 sample because of the smaller size of the starting nanoparticles used to produce the second sample. An x-ray diffractogram for the second sample is shown in Fig. 19.

Example 7 - Orthorhombic  $V_2O_5$  from  $VO_2$  Nanoparticles

30 The starting materials for the heat treatment were  $VO_2$  nanoparticles produced by laser pyrolysis according to the parameters in the second column of Table 3. An x-ray diffractogram of the  $VO_2$ ,

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nano<sup>1</sup>partic<sup>2</sup>les is essentially the same as the x-ray diffractogram in Fig. 11.

The nano<sup>1</sup>partic<sup>2</sup>les were heat treated at a temperature of 202°C with oxygen gas flowed through a 1 inch tube at a rate of 105.6 sccm. The heat treatment was continued for about 16 hours. The resulting nano<sup>1</sup>partic<sup>2</sup>les were single phase crystalline V<sub>2</sub>O<sub>5</sub> nano<sup>1</sup>partic<sup>2</sup>les. The x-ray diffractogram of this material is shown in Fig. 20. From the x-ray diffractogram, it could be determined that the resulting particles were orthorhombic V<sub>2</sub>O<sub>5</sub>.

Additional samples of crystalline V<sub>2</sub>O<sub>5</sub> were made from nano<sup>1</sup>partic<sup>2</sup>les of crystalline VO<sub>2</sub>. The laser pyrolysis conditions to produce the VO<sub>2</sub> nano<sup>1</sup>partic<sup>2</sup>les are presented in Table 5.

Table 5

Phase	VO <sub>2</sub>
Crystal Structure	Monoclinic
Pressure (Torr)	100
Argon F.R. - Win (sccm)	700
Argon F.R. - Sld. (slm)	5.6
Ethylene (sccm)	311
Carrier Gas (sccm)	311(ethyl.)
Oxygen (sccm)	84
Laser Output (watts)	102
Nozzle Size	5/8" x 1/16"

sccm = standard cubic centimeters per minute

slm = standard liters per minute

Argon - Win. = argon flow through inlets 216, 218

Argon - Sld. = argon flow through annular channel 142

The x-ray diffractogram for the VO<sub>2</sub> nano<sup>1</sup>partic<sup>2</sup>les is shown in Fig. 21. Three sample of the VO<sub>2</sub> nano<sup>1</sup>partic<sup>2</sup>les were subjected to heat treatment. All

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three samples were treated for 17 hours in the 1 inch quartz tube with an flow of inert gas (Ar) of 103 sccm. Samples 1, 2 and 3, in addition, had O<sub>2</sub> flow rates of 4.8 sccm, 10.1 sccm and 20.9 sccm, respectively.

5 Samples 1 and 2 were heated at 224°C while sample 3 was heated at a temperature of 221°C. The x-ray diffractograms of the three samples are shown in Figs. 22-24, respectively.

Example 8 - 2-D V<sub>2</sub>O<sub>5</sub> from VO<sub>2</sub> Nanoparticles

10 The initial VO<sub>2</sub> nanoparticles were from the same batch of nanoparticles produced by laser pyrolysis described in Example 7 with parameters given in the second column of values in Table 3. The VO<sub>2</sub> nanoparticles were heated at 105°C for about 21 hours.

15 During heating, O<sub>2</sub> was flowed through the tube at a rate of 106 sccm. The resulting particles had a significant portion of 2-D crystalline V<sub>2</sub>O<sub>5</sub> with a significant fraction of the particles remaining as crystalline VO<sub>2</sub>. The x-ray diffractogram is shown in Fig. 25.

20 Example 9 - 2-D V<sub>2</sub>O<sub>5</sub> from Amorphous V<sub>2</sub>O<sub>5</sub> Nanoparticles

The initial amorphous V<sub>2</sub>O<sub>5</sub> nanoparticles were from the same batch of nanoparticles produced by laser pyrolysis described in Example 6 with parameters given in the second column of values in Table 2. The amorphous V<sub>2</sub>O<sub>5</sub> nanoparticles were heated at 105°C for about 21 hours. During heating, O<sub>2</sub> was flowed through the tube at a rate of 106 sccm. The resulting particles had an x-ray diffractogram characteristic of 2-D crystalline V<sub>2</sub>O<sub>5</sub>, as shown in Fig. 26.

30 Comparative Example 1- Commercial V<sub>6</sub>O<sub>13</sub>

Commercial V<sub>6</sub>O<sub>13</sub> was purchased from Alfa Aesar, a Johnson Matthey Company, Ward Hill, MA. A 7.8 quantity of the commercial V<sub>6</sub>O<sub>13</sub> powder was processed into a cathode and tested in a lithium battery,

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described above. Over the course of the 170 hour test, the battery was discharged three times. The initial voltage was 3.54 V. The cell had a discharge capacity of 246.2 Ah/kg and an energy density of the cathode active material of 610.1 Wh/kg. This energy density compared with a theoretical maximum value of 890 Wh/kg based on the reversible intercalation of up to 8 lithium ions per unit cell of vanadium oxide.

Example 10 - VO<sub>2</sub> Nanoparticles

Nanoscale VO<sub>2</sub> particles were produced by laser pyrolysis according to the parameters in column 1 of Table 3. As noted above, an analysis of the TEM photo for the VO<sub>2</sub> nanoparticles reveals an average particle size of about 22 nm. A plot of voltage as a function of time during the discharge/charge cycling is shown in Fig. 27. A battery produced with these materials yielded a Discharge Capacity of 249 Ah/kg and an energy density of 549 Wh/kg. The Discharge Capacity and Energy Density are nearly twice the values obtained from larger VO<sub>2</sub> particles. These values are higher than the theoretical maximum-stoichiometric energy density of 390 Wh/kg for VO<sub>2</sub> for the bulk material at 25°C. See, K. West et al., "Vanadium Oxides as Electrode Materials for Rechargeable Lithium Cells," J. of Power Sources 20:165-172 (1987), incorporated herein by reference.

Example 11 - Single Phase 2D-V<sub>2</sub>O<sub>5</sub> Nanoparticles

Single phase 2-D V<sub>2</sub>O<sub>5</sub> nanoparticles were produced by laser pyrolysis according to the parameters in column 4 of Table 2. As noted above, an analysis of a TEM photo of the 2-D V<sub>2</sub>O<sub>5</sub> nanoparticles reveals an average particle size of about 20 nm. A battery produced with these materials yielded a Discharge Capacity of 146 Ah/kg and an Energy Density of 380 Wh/kg.

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Example 12 - Amorphous V<sub>2</sub>O<sub>5</sub> Nanoparticles

Single phase amorphous V<sub>2</sub>O<sub>5</sub> nanoparticles were produced by laser pyrolysis according to the parameters in the first column of Table 2. As noted above, an analysis of a TEM photo of the amorphous V<sub>2</sub>O<sub>5</sub> nanoparticles reveals an average particle size of about 200 nm for the amorphous V<sub>2</sub>O<sub>5</sub> nanoparticles used to form the cathode. Two batteries produced with these materials yielded Discharge Capacities of 186.1 Ah/kg and 177.3 Ah/kg, and Energy Densities of 476 Wh/kg and 446.2 Wh/kg.

Example 13 - Mixed Phase V<sub>6</sub>O<sub>13</sub> / VO<sub>2</sub> Nanoparticles

Mixed phase crystalline V<sub>6</sub>O<sub>13</sub> / VO<sub>2</sub> nanoparticles were produced by laser pyrolysis according to the parameters in the first column of Table 4. As noted above, an analysis of a TEM photo of the mixed phase nanoparticles reveals an average particle size of about 20 to about 30 nm for the mixed phase V<sub>6</sub>O<sub>13</sub> / VO<sub>2</sub> nanoparticles. A battery produced with these materials yielded a Discharge Capacity of 174 Ah/kg and an Energy Density of 403 Wh/kg.

Example 14 - Crystalline V<sub>2</sub>O<sub>5</sub> Nanoparticles

The crystalline V<sub>2</sub>O<sub>5</sub> nanoparticles were produced by further processing nanoparticles produced by laser pyrolysis in an oven with an oxygen atmosphere, as described above. Three types of nanoparticles produced by laser pyrolysis were used for further processing. The nanoparticles of Sample A are the particles described above in Example 6 that were produced from amorphous V<sub>2</sub>O<sub>5</sub> particles. The nanoparticles of samples B were the particles described above as the first sample of Example 7 that were produced from crystalline VO<sub>2</sub> nanoparticles.

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The crystalline V<sub>2</sub>O<sub>5</sub> nanoparticles were formed into batteries. The crystalline V<sub>2</sub>O<sub>5</sub> nanoparticles from Sample A yielded a Discharge Capacity of 399 Ah/kg and a Energy Density of 1005 Wh/kg while the crystalline V<sub>2</sub>O<sub>5</sub> nanoparticles from Sample B yielded a Discharge Capacity of 370 Ah/kg and an Energy Density of 919 Wh/kg. Note that crystalline V<sub>2</sub>O<sub>3</sub> nanoparticles have resulted in an Energy Density greater than 1000 Wh/kg, which is greater than a factor of two larger than estimated theoretical maximum values for bulk V<sub>2</sub>O<sub>5</sub>.

A third sample was produced by laser pyrolysis using conditions presented in Table 6.

Table 6

Pressure (Torr)	230
Argon - Win (sccm)	700
Argon - Sld. (slm)	5.6
Ethylene (sccm)	2680
Carrier Gas (Argon) sccm	980
Oxygen (sccm)	700
Laser Output (watts)	180
Nozzle Size	5/8" x 1/8"

The third sample was also further processed in an oven. The nanoparticles were heated for 16 hours at 227°C with an O<sub>2</sub> flow rate of 105.6 sccm. Processing these heat treated particles into a battery as described above, a Discharge Capacity of 438 Ah/kg and an Energy Density of 1121 Wh/kg were measured.

Example 15 - Summary of Oven Treated Nanoparticles And Nanoparticles Produced Directly by Laser Pyrolysis

This example summarizes a set of measurements taken with different batches of vanadium oxide nanoparticles. The nanoparticles were either made directly with laser pyrolysis (Table 7A) or with

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additional heating in an oven under oxidizing conditions (Table 7B).

Table 7A  
Vanadium Oxide Properties

Material	Discharge Capacity (Ah/kg)	Energy Density (Wh/kg)
Amorphous V <sub>2</sub> O <sub>3</sub>	182	461
VO <sub>2</sub> *	137	328
2D - V <sub>2</sub> O <sub>3</sub> **	146	380
VO <sub>2</sub>	235	519
VO <sub>2</sub>	249	549
VO <sub>2</sub>	168	377
VO <sub>2.2</sub>	118	270
V <sub>2</sub> O <sub>3</sub>	94	209
Mixed Phase VO <sub>2</sub> /V <sub>2</sub> O <sub>3</sub>	228	510
Amorphous V <sub>2</sub> O <sub>3</sub>	188	445
Mixed Phase - V <sub>2</sub> O <sub>3</sub> /VO <sub>2</sub>	174	403

Two measurements were made with the same nanoparticles. The individual values were 140 Ah/kg and 20 133 Ah/kg (Discharge Capacity), and 323 Wh/kg and 333 Wh/kg (Energy Density).

\*\* Two measurements were made with the same nanoparticles. The individual values were 146 Ah/kg and 146 Ah/kg (Discharge Capacity), and 378 Wh/kg and 381 Wh/kg (Energy Density).

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Table 7B  
Vanadium Oxide Properties - Heat Treated

	Material	Discharge Capacity (Ah/kg)	Energy Density (Wh/kg)
5	Orthorhombic V <sub>2</sub> O <sub>5</sub>	336	848
	Mixed Phase VO <sub>2</sub> /V <sub>2</sub> O <sub>5</sub>	297	721
	Orthorhombic V <sub>2</sub> O <sub>5</sub>	399	1005
	Orthorhombic V <sub>2</sub> O <sub>5</sub>	370	919
	2-D V <sub>2</sub> O <sub>5</sub>	292	738
	Mixed Phase 2D V <sub>2</sub> O <sub>5</sub> /VO <sub>2</sub>	304	751
		438	1121

The embodiments described above are intended  
 15 to be representative and not limiting. Additional  
 embodiments of the invention are within the claims. As  
 will be understood by those skilled in the art, many  
 changes in the methods and apparatus described above may  
 20 be made by the skilled practitioner without departing  
 from the spirit and scope of the invention, which should  
 be limited only as set forward in the claims which  
 follow.

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WHAT IS CLAIMED IS:

1. A collection of particles comprising vanadium oxide, the measurements along the principle axes of the particles are each about 1000 nm or less for at least about 95 percent of the particles.
2. The collection of particles of claim 1 having an average diameter from about 5 nm to about 100 nm.
3. The collection of particles of claim 1 having an average diameter from about 5 nm to about 50 nm.
4. The collection of particles of claim 1 wherein the vanadium oxide has a stoichiometry of  $\text{VO}_2$ .
5. The collection of particles of claim 1 wherein the vanadium oxide has a stoichiometry of  $\text{V}_2\text{O}_5$ .
6. The collection of particles of claim 1 wherein the vanadium oxide has a stoichiometry of  $\text{V}_6\text{O}_{13}$ .
7. The collection of particles of claim 1 wherein the vanadium oxide is crystalline.
8. The collection of particles of claim 1 wherein 95 percent of the vanadium oxide nanoparticles have a diameter greater than about 50 percent of the average diameter and less than about 150 percent of the average diameter.
9. A method of producing vanadium oxide nanoparticles comprising the step of pyrolyzing a molecular stream comprising a vanadium precursor, an oxidizing agent and a radiation absorbing gas in a reaction chamber, where the pyrolysis is driven by heat absorbed from a laser beam.
10. The method of claim 9 wherein the vanadium oxide nanoparticles have an average diameter from about 5 nm to about 150 nm.
11. An apparatus comprising:
  - (a) a reaction chamber isolated from the ambient atmosphere;

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- (b) a reactant gas inlet defining a path of a molecular stream, the inlet being connected to a source of vanadium precursor, an oxidizing agent and a laser absorbing gas;
- (c) a laser beam path intersecting the path of the molecular stream; and
- (d) a product outlet.

12. The apparatus of claim 11 wherein the vanadium precursor is  $\text{VOCl}_3$ , and the oxidizing agent is  $\text{O}_2$ .

13. The apparatus of claim 11 wherein the reactant gas inlet is elongated in one dimension.

14. A process for converting nanoparticles of vanadium oxide to other forms of vanadium oxide comprising the step of heating the nanoparticles of vanadium oxide in an oxidizing or inert atmosphere at a temperature at least about  $300^\circ\text{C}$  below the melting point of both the nanoparticles of vanadium oxide and the other forms of vanadium oxide.

15. The process of claim 14 wherein the temperature is between about  $60^\circ\text{C}$  and about  $500^\circ\text{C}$ .

16. The process of claim 14 wherein the heating is performed in an oxidizing atmosphere, wherein the oxidizing atmosphere comprises between about 1 percent oxidizing gas and about 99 percent oxidizing gas by partial pressure.

17. The process of claim 14 wherein the other forms of vanadium oxide comprise 2-D crystalline  $\text{V}_2\text{O}_5$  or crystalline  $\text{V}_2\text{O}_5$ .

18. The process of claim 14 wherein the nanoparticles of vanadium oxide have an average diameter from about 5 nm to about 150 nm.

19. Vanadium oxide nanoparticles formed by heating in an oxidizing or inert atmosphere, vanadium oxide nanoparticles of a different form.

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20. The vanadium oxide nanoparticles of claim 19 wherein the vanadium oxide nanoparticles of a different form have an average diameter from about 5 nm to about 150 nm.
21. The vanadium oxide nanoparticles of claim 19 wherein the vanadium oxide nanoparticles formed by heating have a higher oxygen to vanadium ratio than the vanadium oxide nanoparticles of a different form.
22. The vanadium oxide nanoparticles of claim 19 wherein the vanadium oxide nanoparticles formed by heating comprise  $V_2O_5$ .
23. A process for forming vanadium oxide particles comprising the step of heating particles of vanadium oxide with a lower oxygen to vanadium ratio than the vanadium oxide particles to be formed in an oxidizing atmosphere at a temperature at least about 300°C below the melting point of both the vanadium oxide particles to be heated and the product vanadium oxide particles to be formed.
24. The process of claim 23 wherein the temperature is between about 60°C and about 800°C.
25. The process of claim 23 wherein the initial vanadium oxide particles have an average diameter from about 5 nm to about 1000 nm.
26. A process for forming crystalline  $V_2O_5$  comprising the step of heating amorphous  $V_2O_5$  at a temperature at least about 300°C below the melting point of both the amorphous  $V_2O_5$  and the crystalline  $V_2O_5$ .
27. The process of claim 26 wherein the temperature is between about 60°C and about 800°C.
28. The process of claim 26 wherein the amorphous  $V_2O_5$  particles have an average diameter from about 5 nm to about 1000 nm.

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29. A cathode composition comprising vanadium oxide particles having an average diameter less than about 1000 nm and a binder.
30. The cathode composition of claim 29 wherein the vanadium oxide particles have an average diameter from about 50 nm to about 5 nm.
31. The cathode composition of claim 29 wherein the binder comprises polyvinylidene fluoride, polyethylene oxide, polyethylene, polypropylene, polytetrafluoroethylene, polyacrylates or mixtures or copolymers thereof.
32. The cathode composition of claim 29 further comprising supplementary electrically conductive particles.
33. The cathode composition of claim 29 wherein the cathode comprises from about 60 percent by weight to about 98 percent by weight vanadium oxide particles.
34. A battery comprising an anode, a cathode comprising vanadium oxide particles having an average diameter less than about 1000 nm and a binder, and a separator element disposed between the anode and cathode.
35. The battery of claim 34 wherein the anode comprises lithium metal.
36. The battery of claim 34 wherein the anode comprises a composition that intercalates lithium.
37. A battery comprising an anode, an electrolyte, a cathode and a separator element disposed between the anode and the cathode, the electrolyte comprising lithium ions and the cathode comprising nanoparticles of intercalation type electroactive material and a binder, wherein the electroactive material in the cathode exhibits an energy density greater than about 900 Wh/kg during discharge of the battery.

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38. The battery of claim 37 wherein the battery is a secondary battery.
39. The battery of claim 37, wherein the electroactive material in the cathode exhibits an energy density from about 950 Wh/kg to about 1200 Wh/kg.
40. The battery of claim 37 wherein the electroactive nanoparticles comprise vanadium oxide.
41. The battery of claim 37 wherein the electroactive material in the anode comprises a composition that intercalates lithium.

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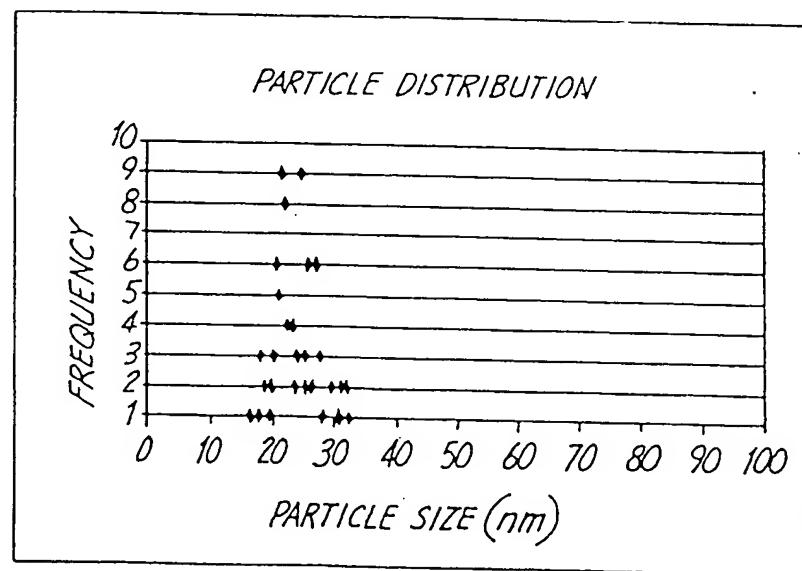
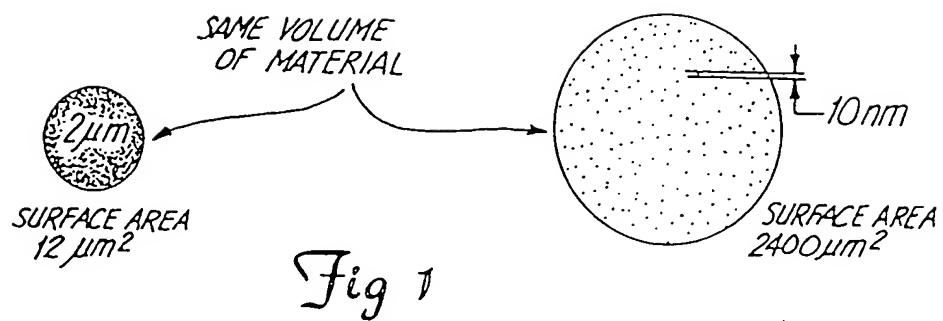
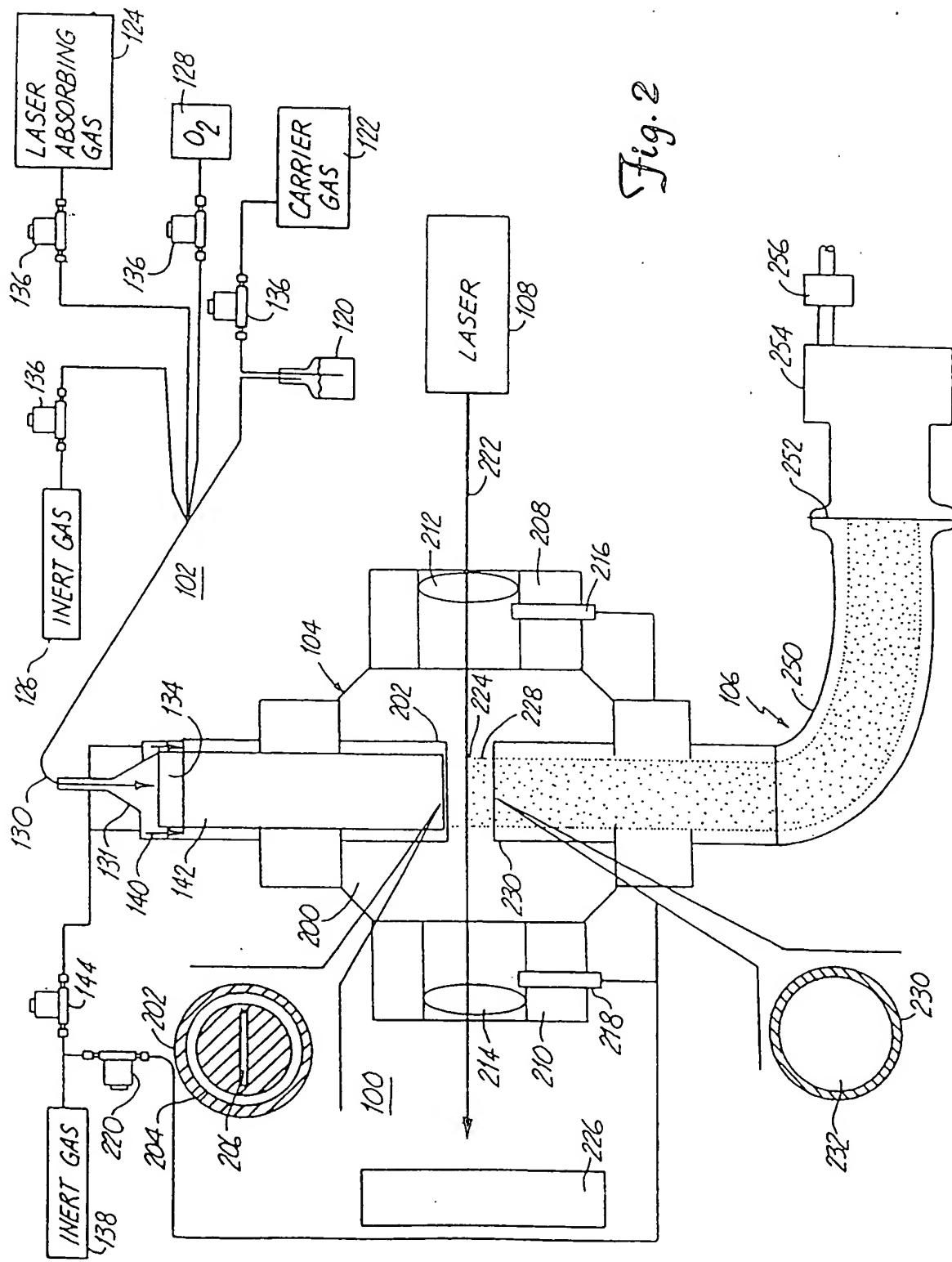


Fig 14

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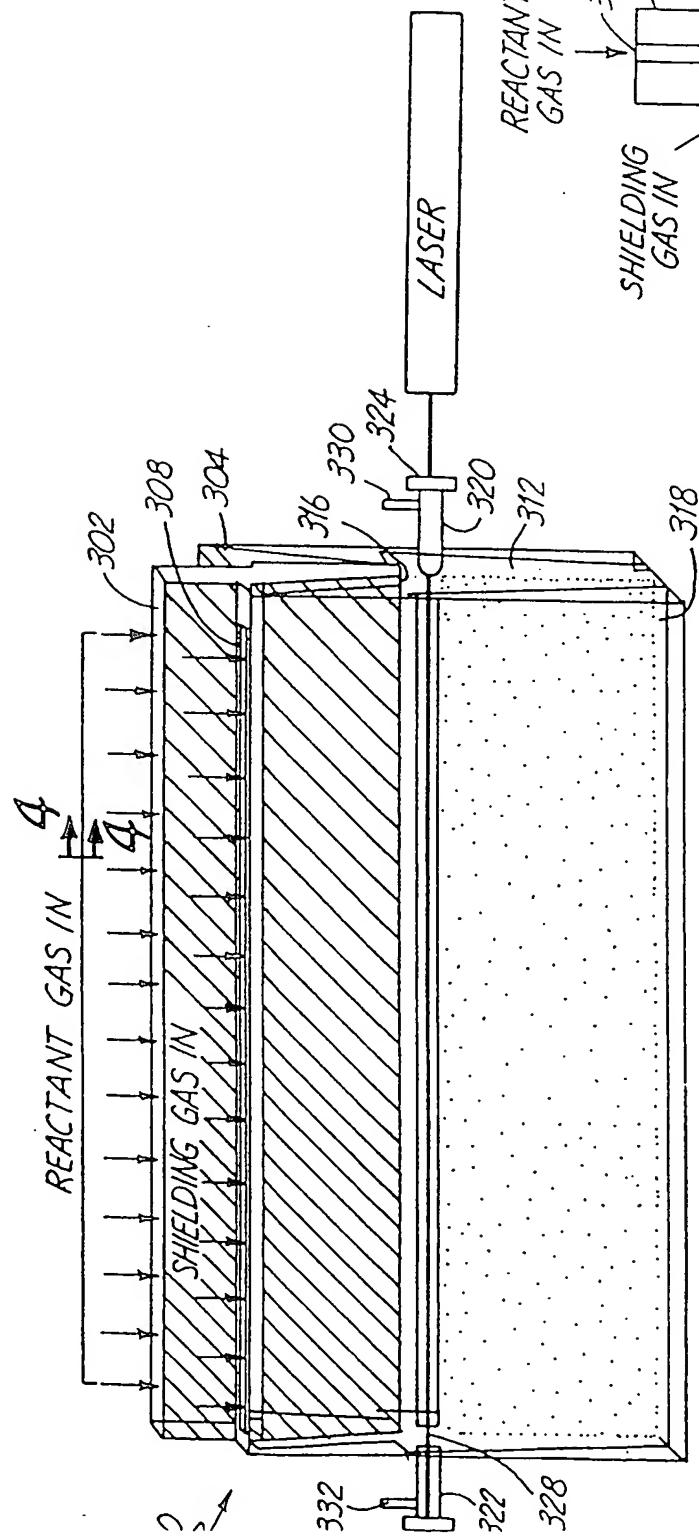


Fig. 3

NANO PARTICLES OUT

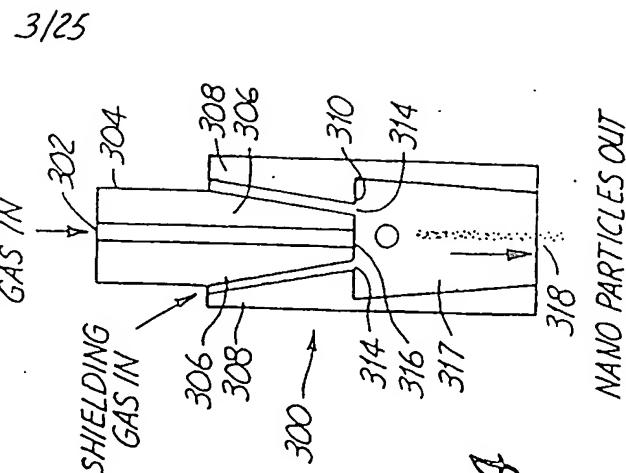


Fig. 4

NANO PARTICLES OUT

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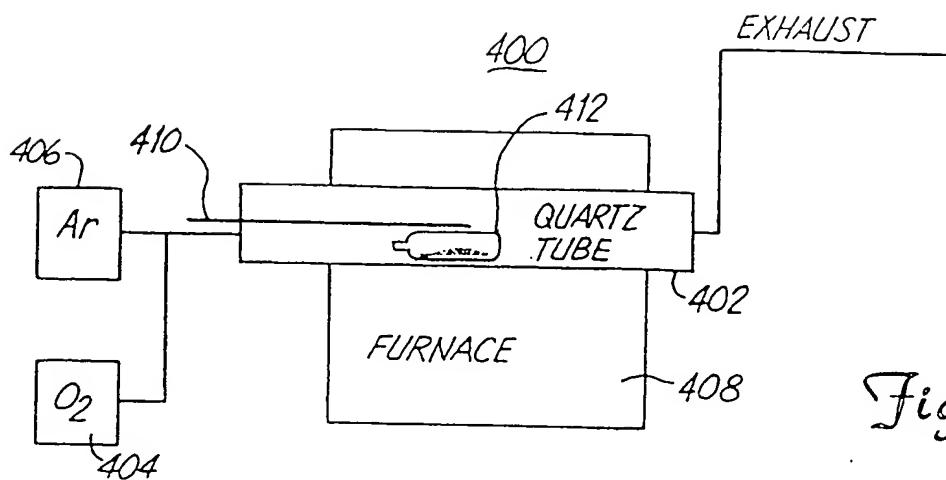


Fig. 5

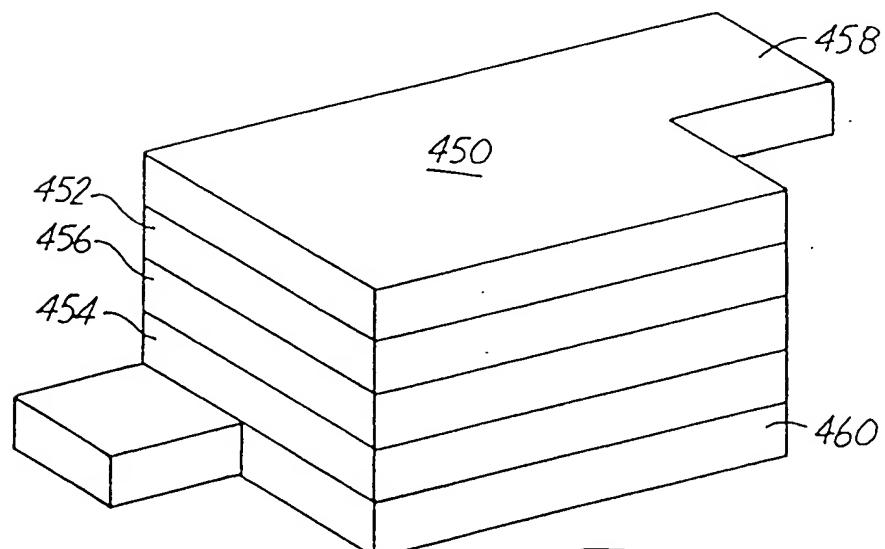


Fig. 6

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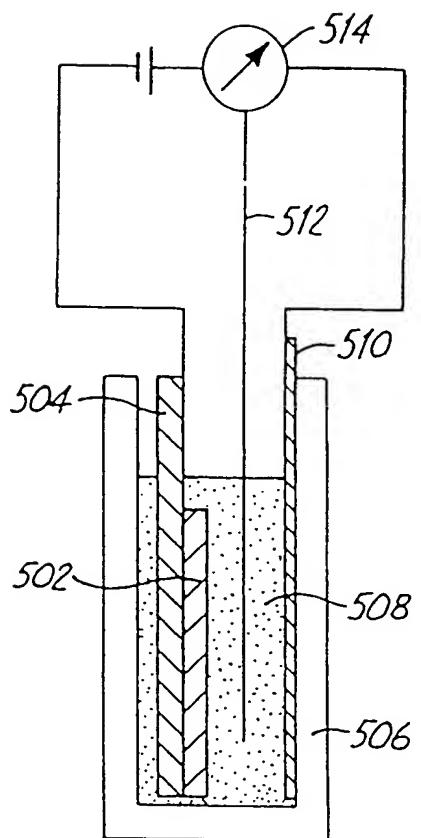
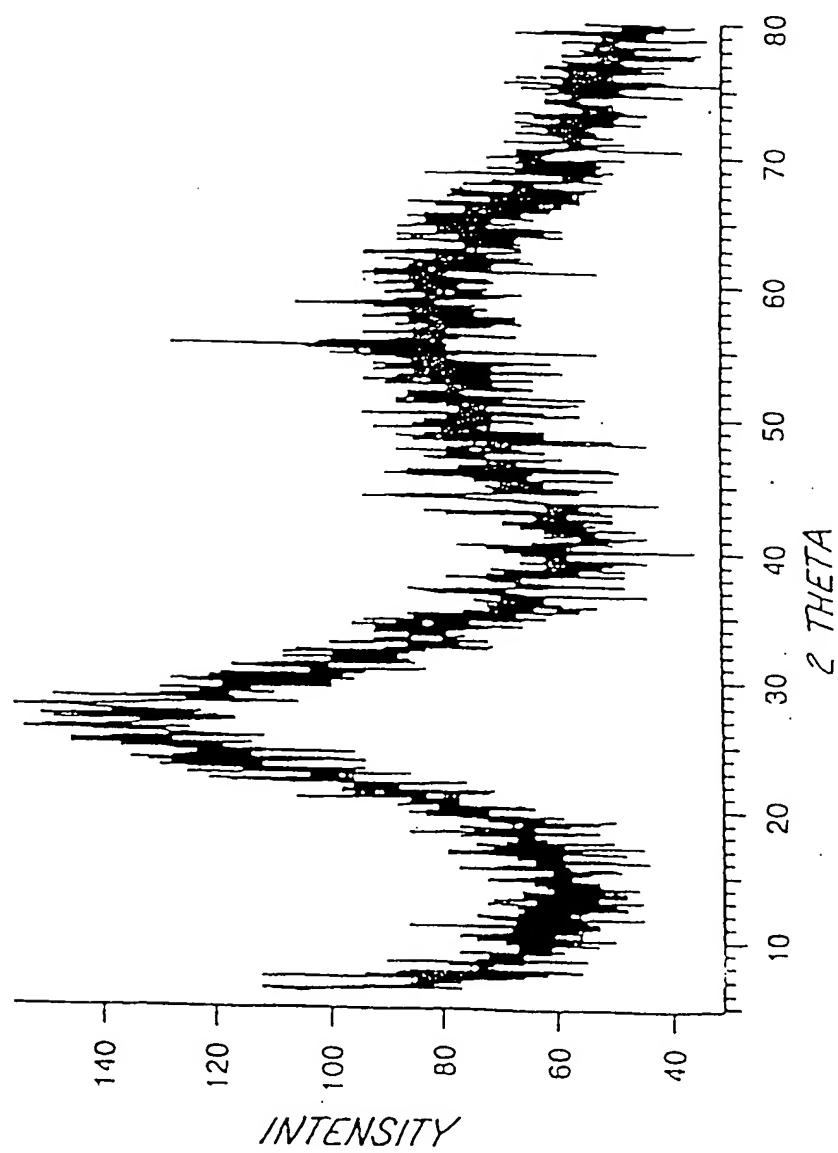


Fig. 7

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Fig. 8



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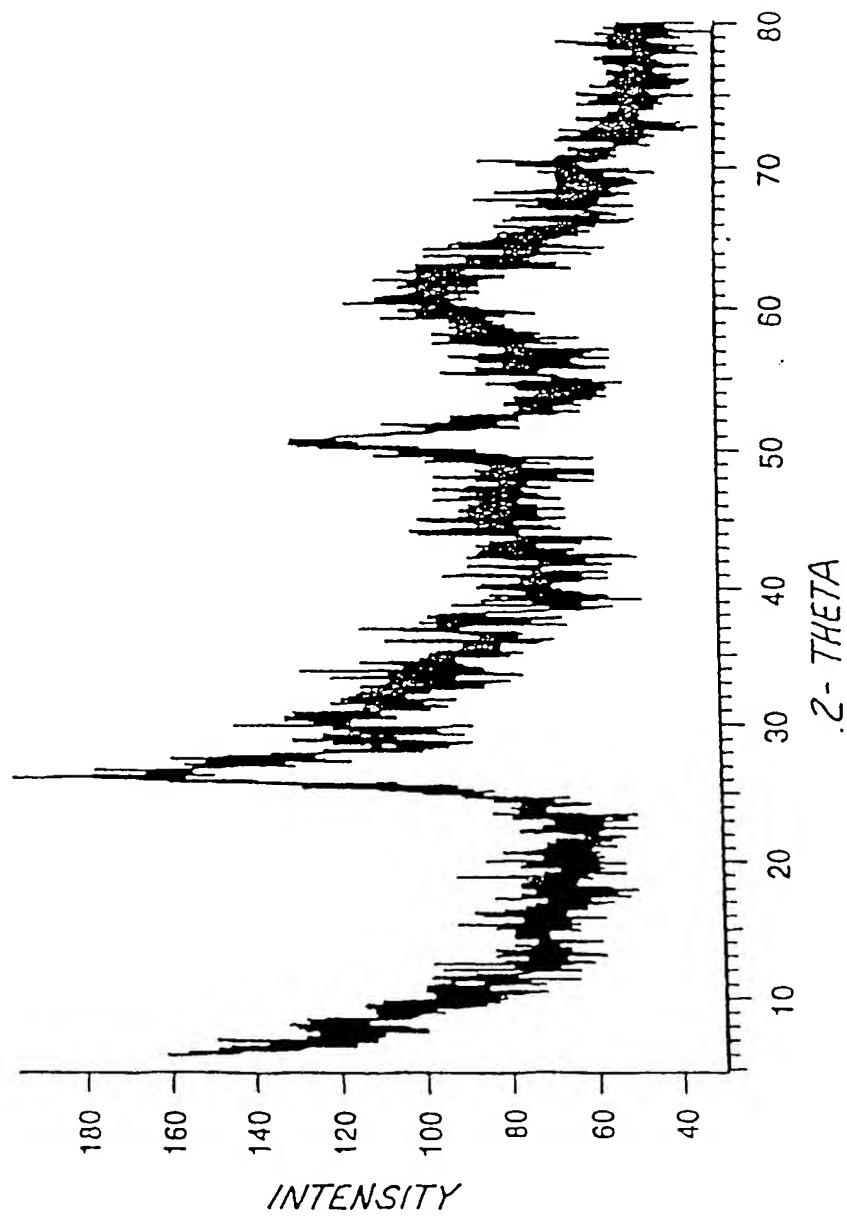
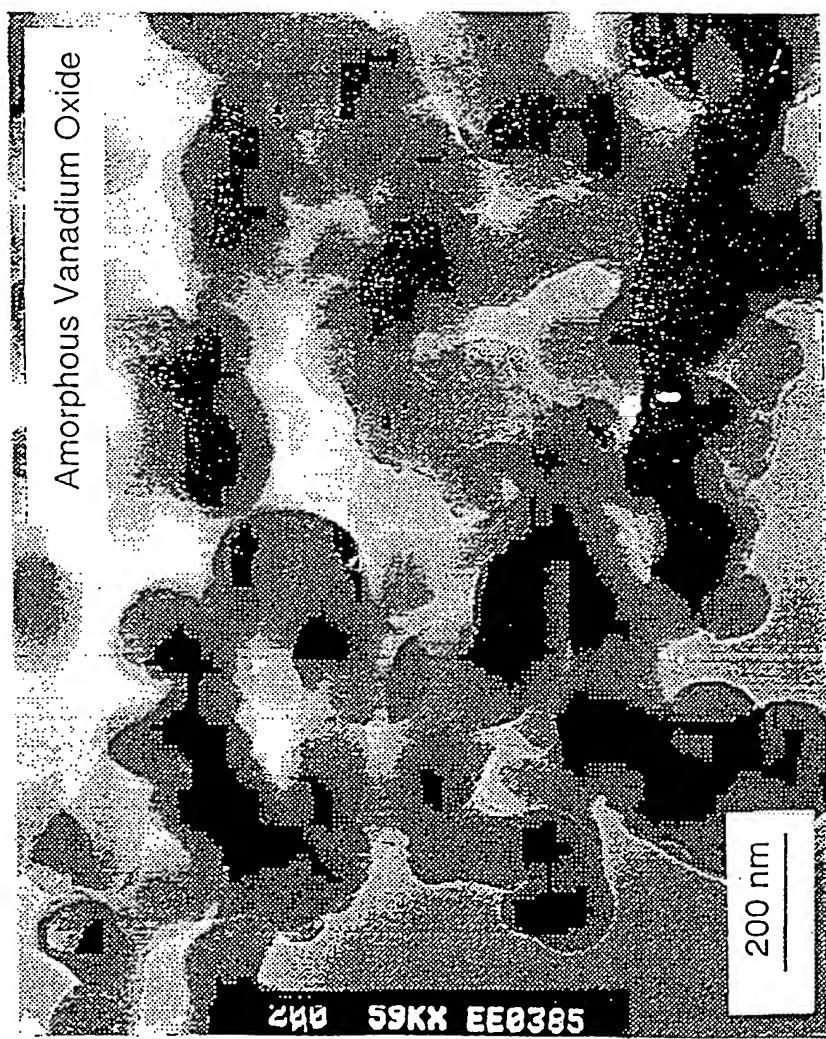


Fig. 9

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Fig. 10



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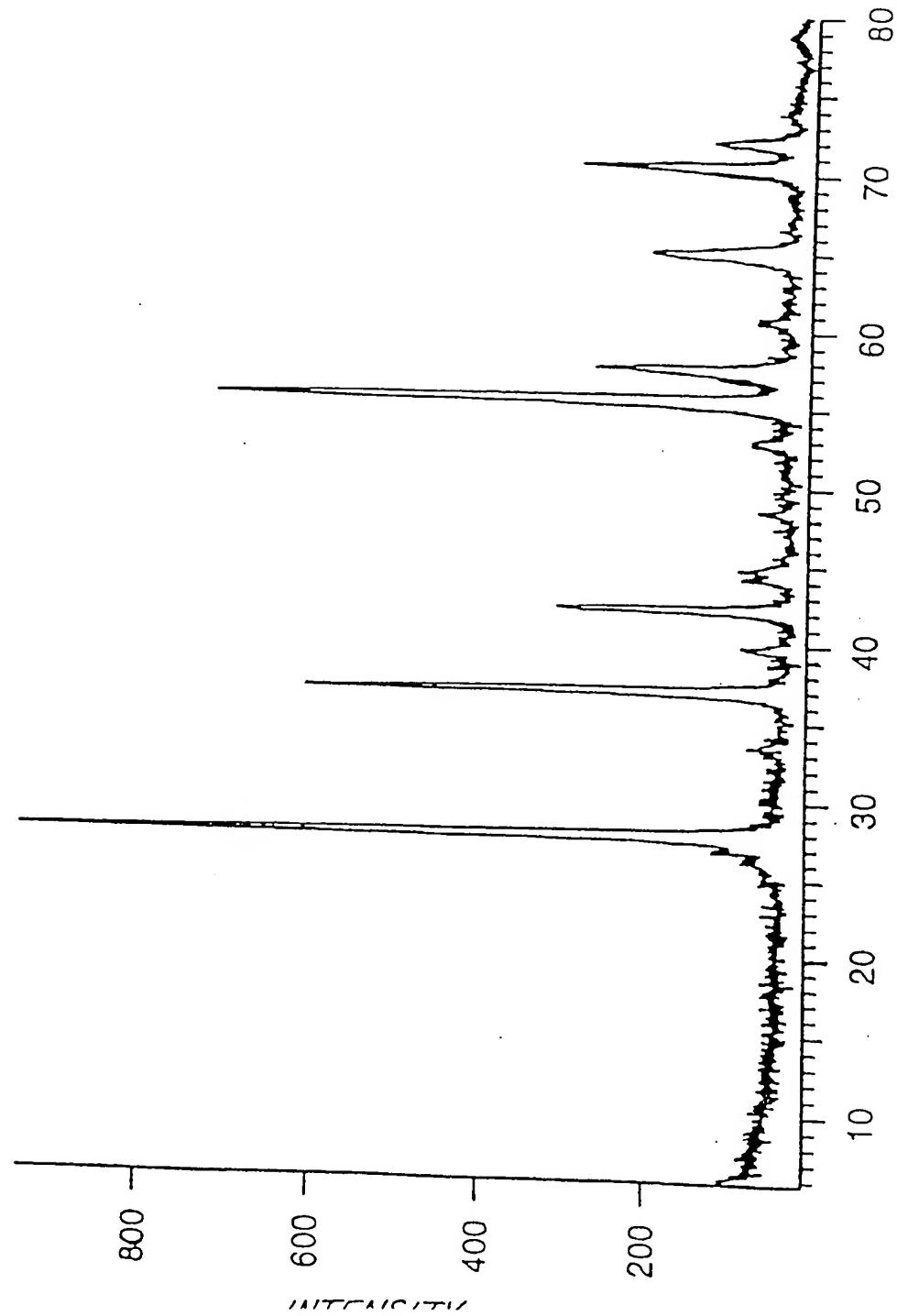
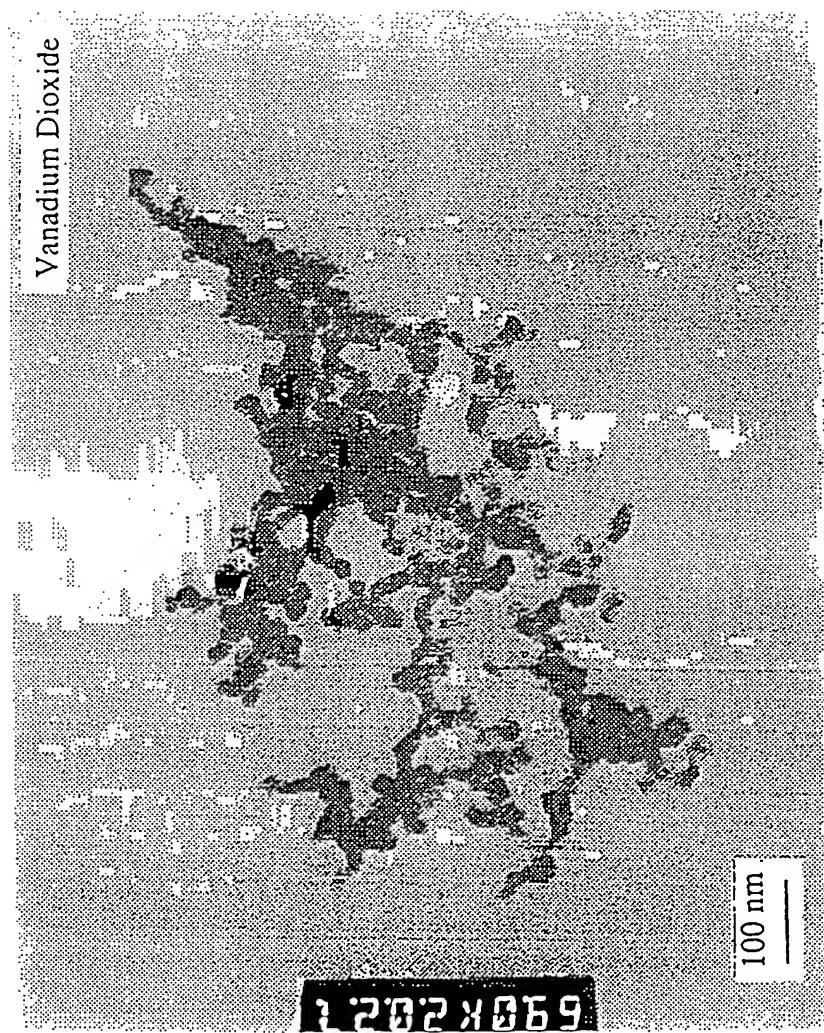


Fig. 11

2 THETA

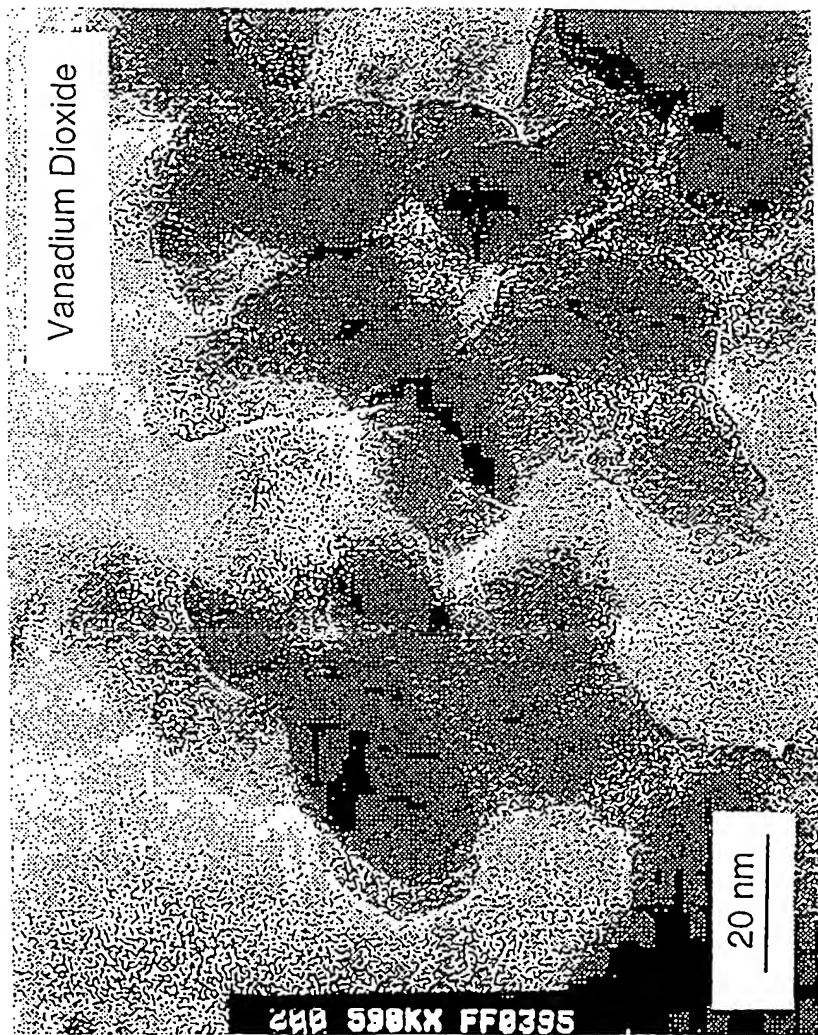
10/25

Fig. 12



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Fig. 13



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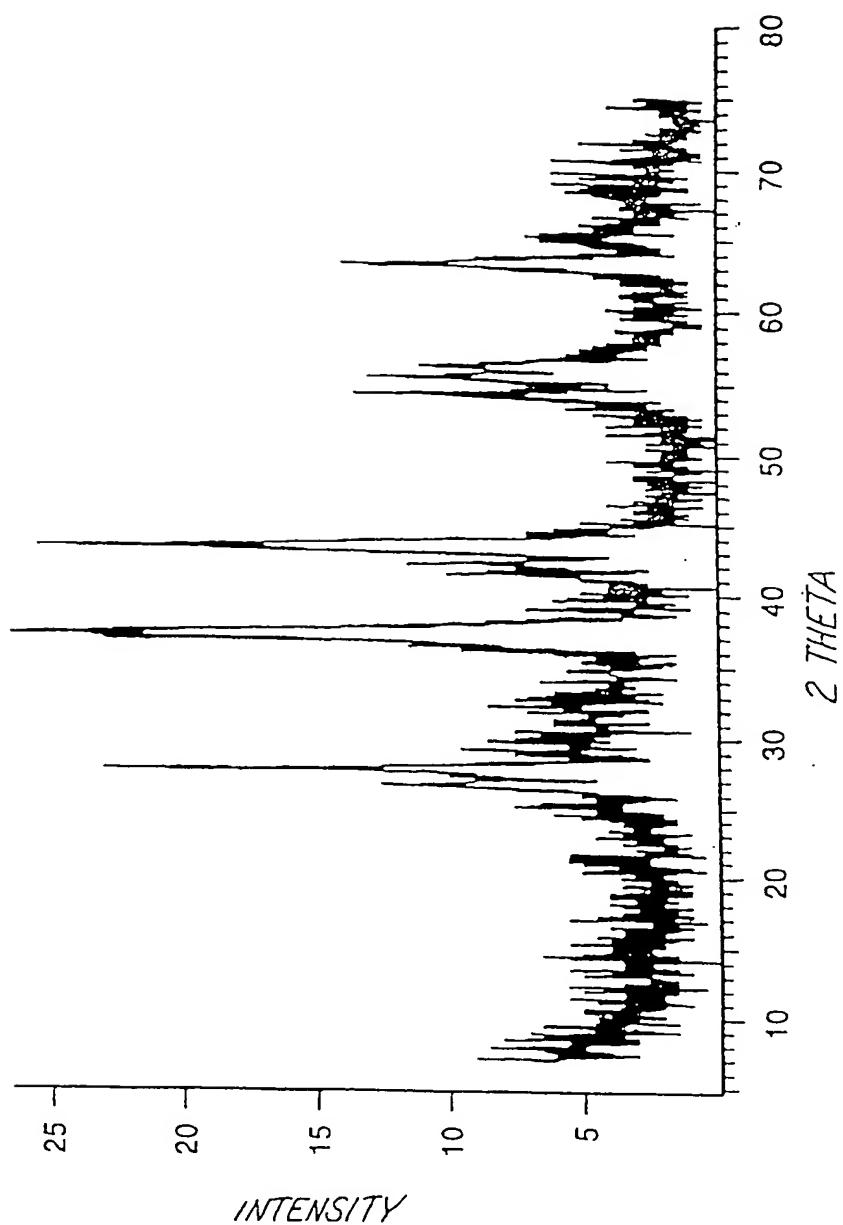


Fig. 15

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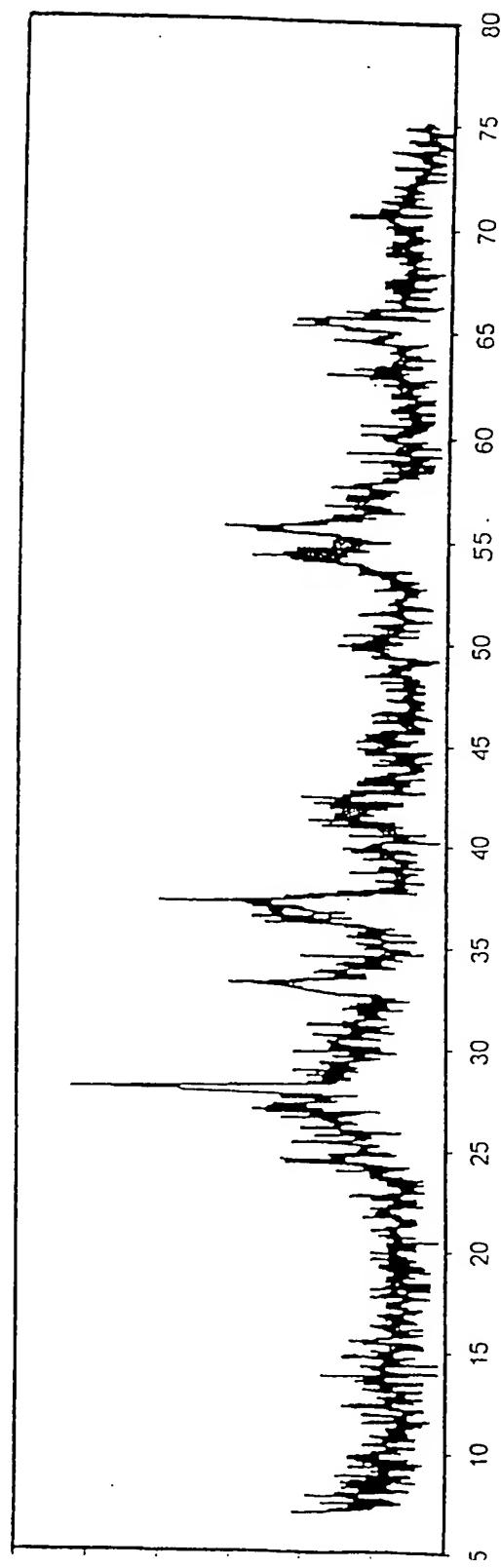


Fig. 17

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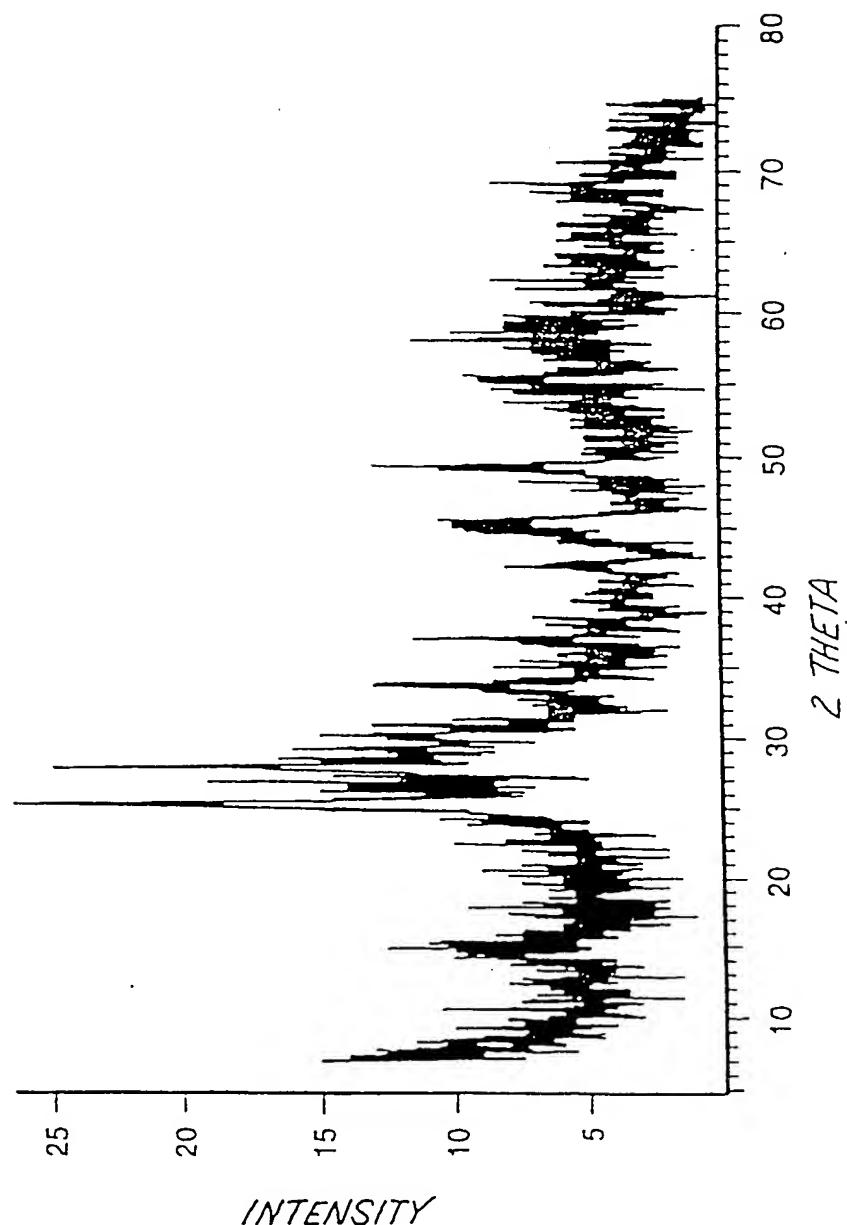
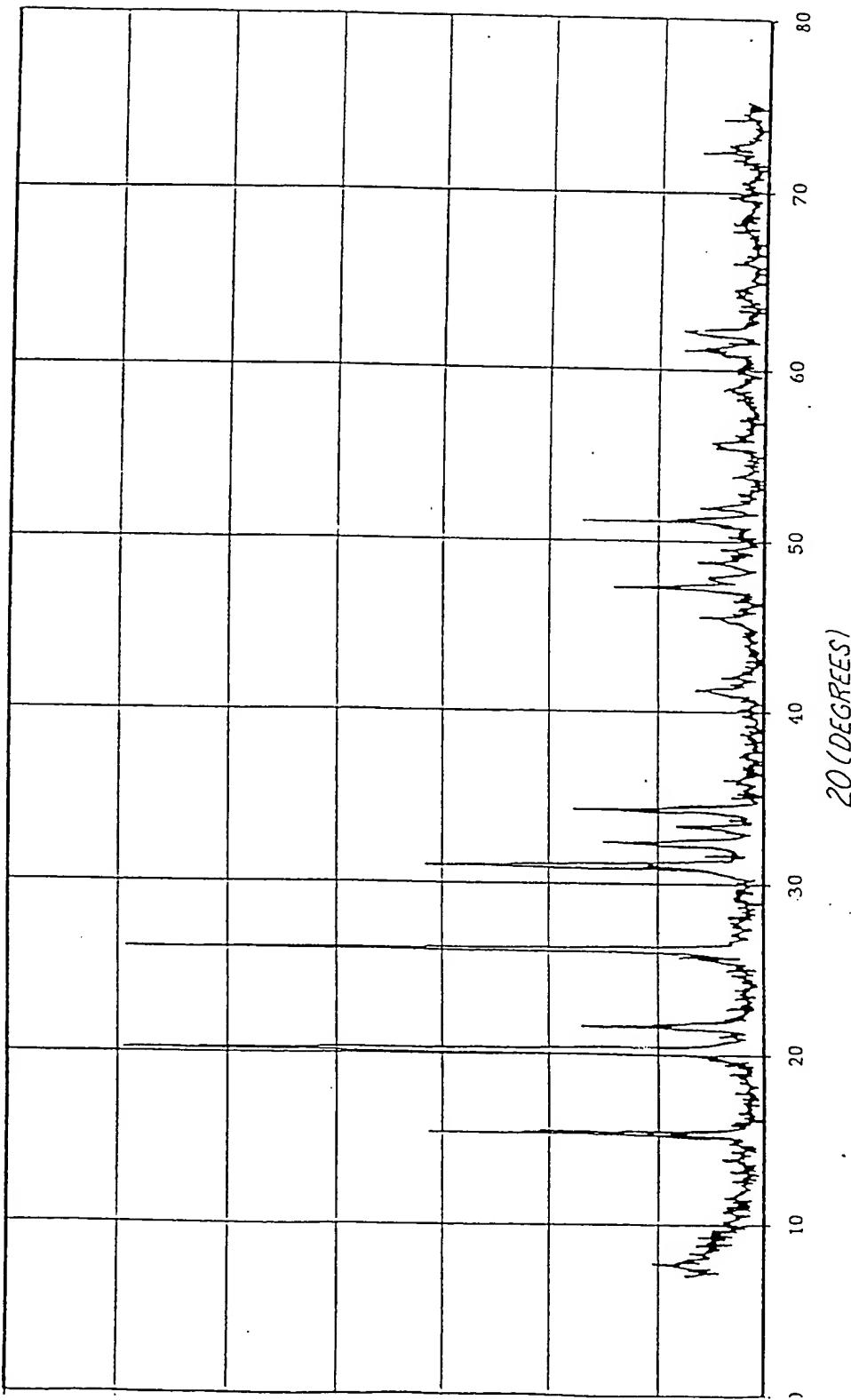


Fig. 16

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BATTERY CAPACITY: 398.7 mAh/g

Fig. 18



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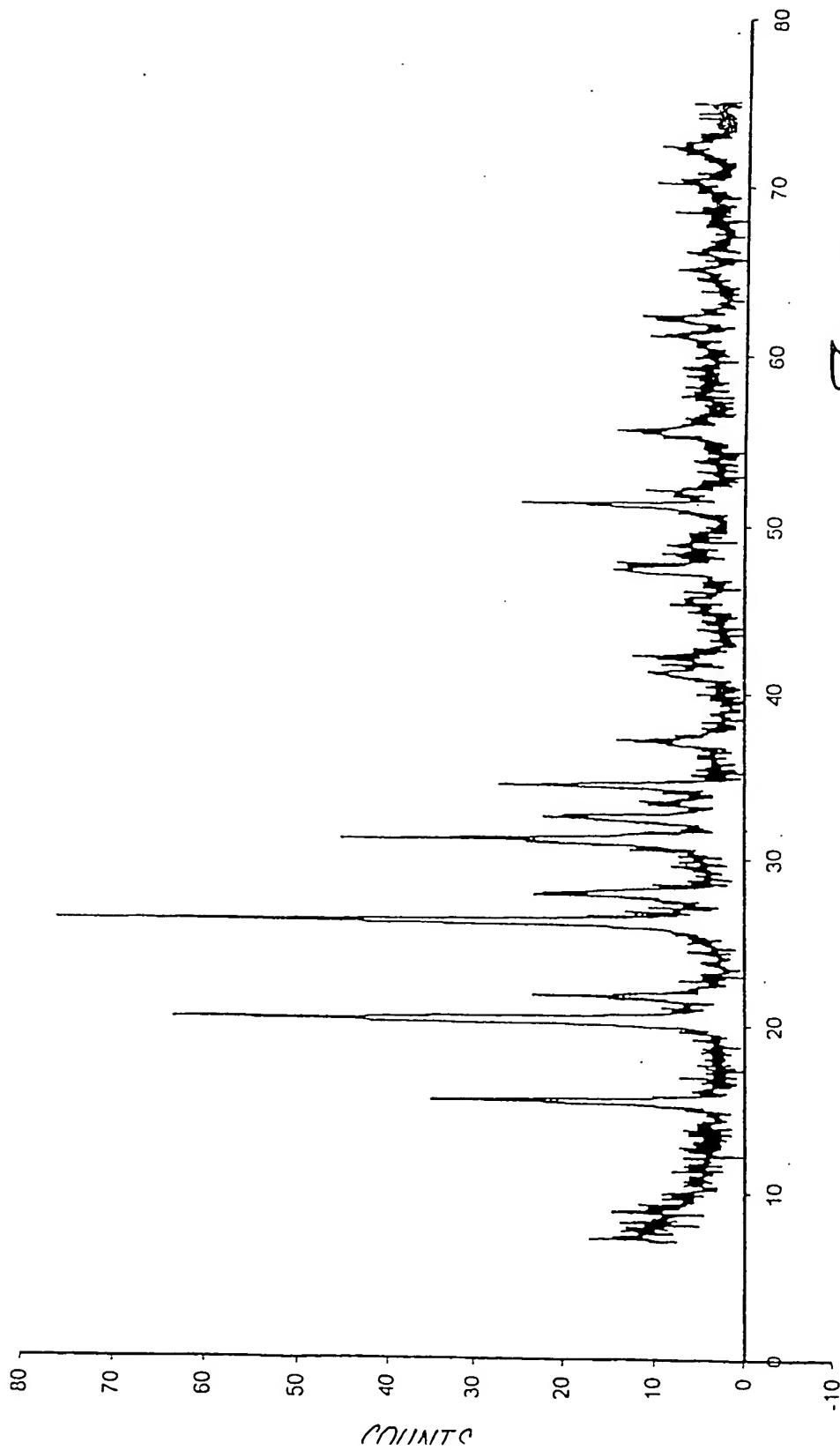


Fig. 19

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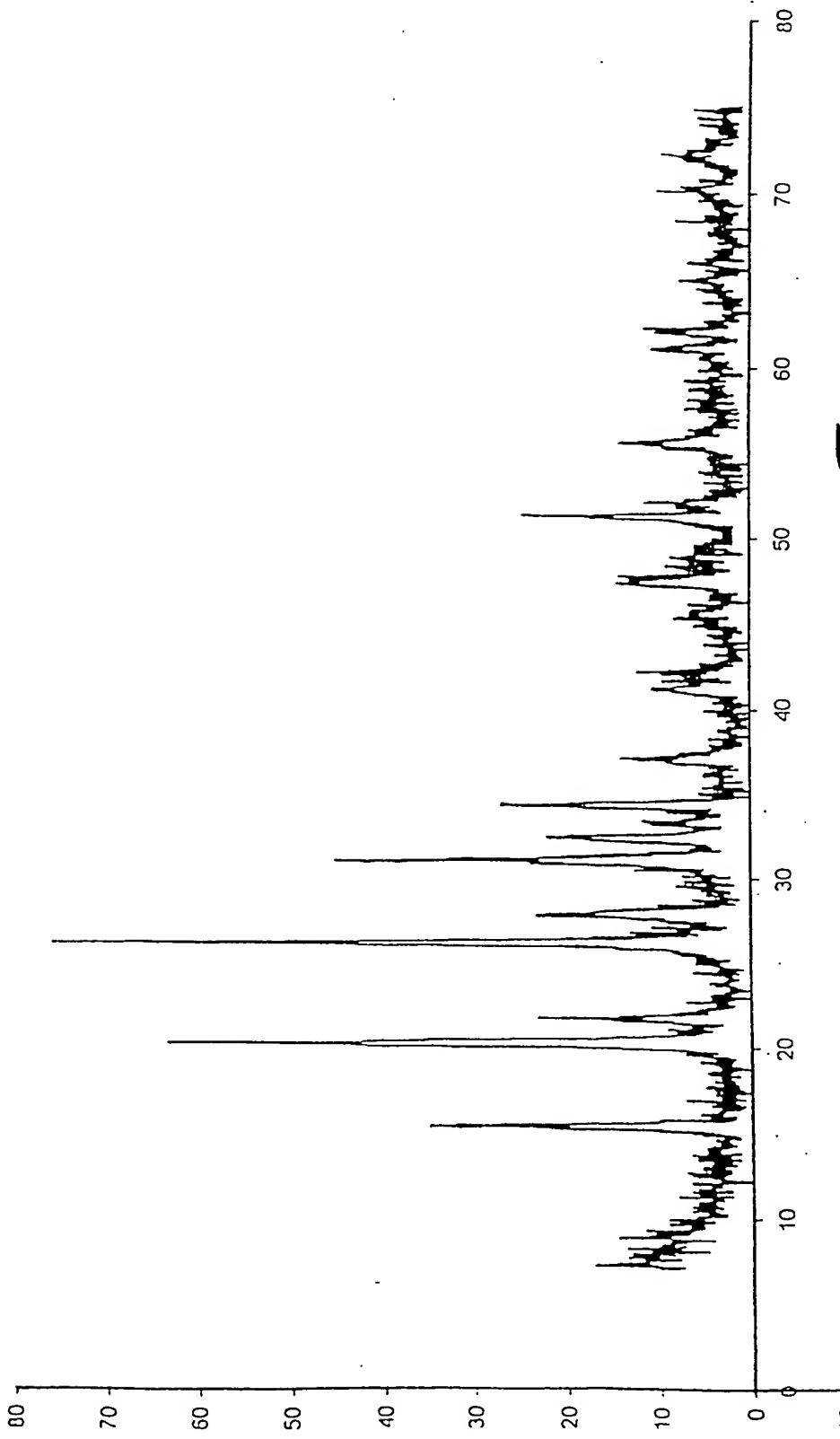


Fig. 20

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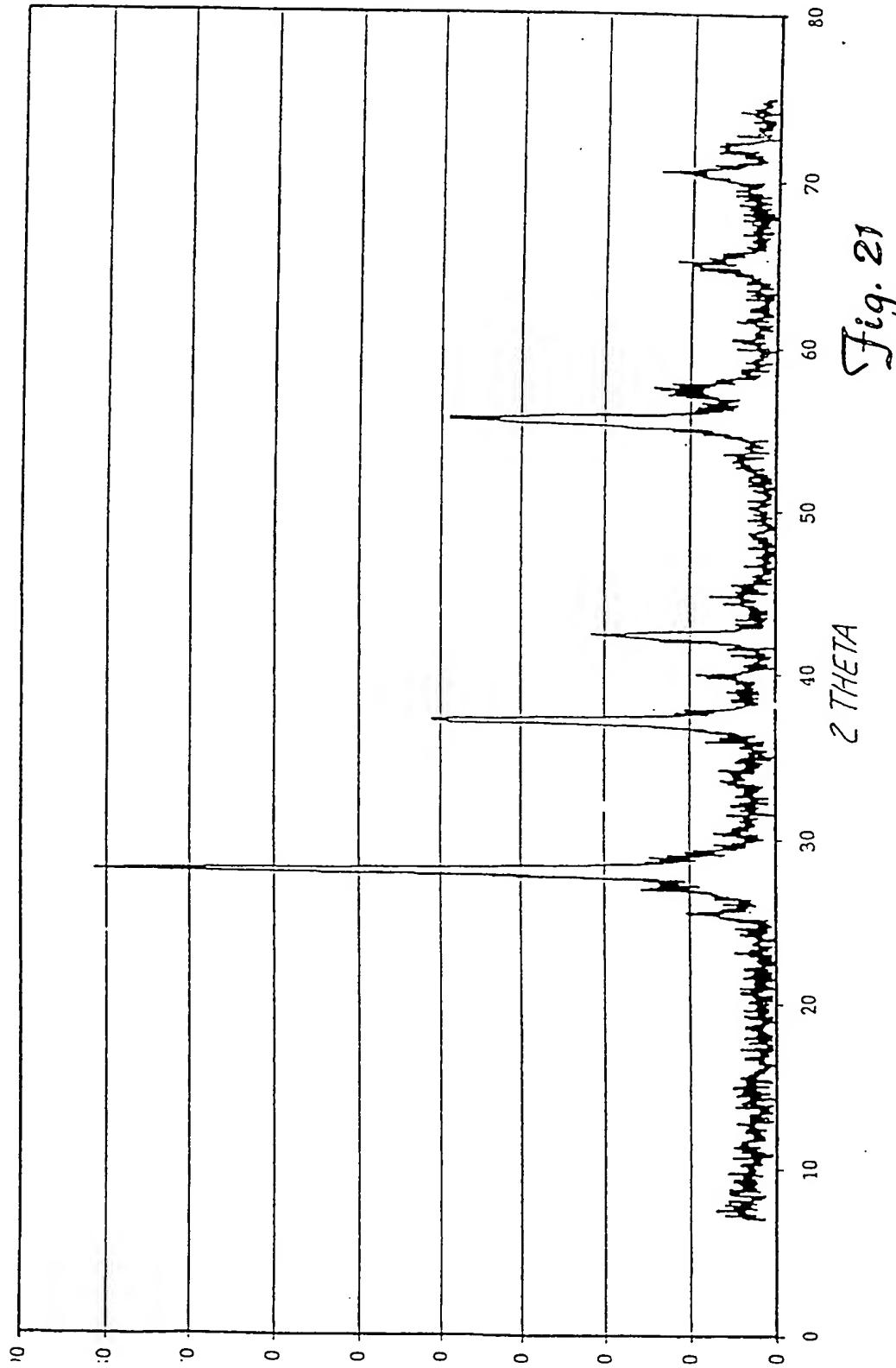


Fig. 21

 $2\theta$

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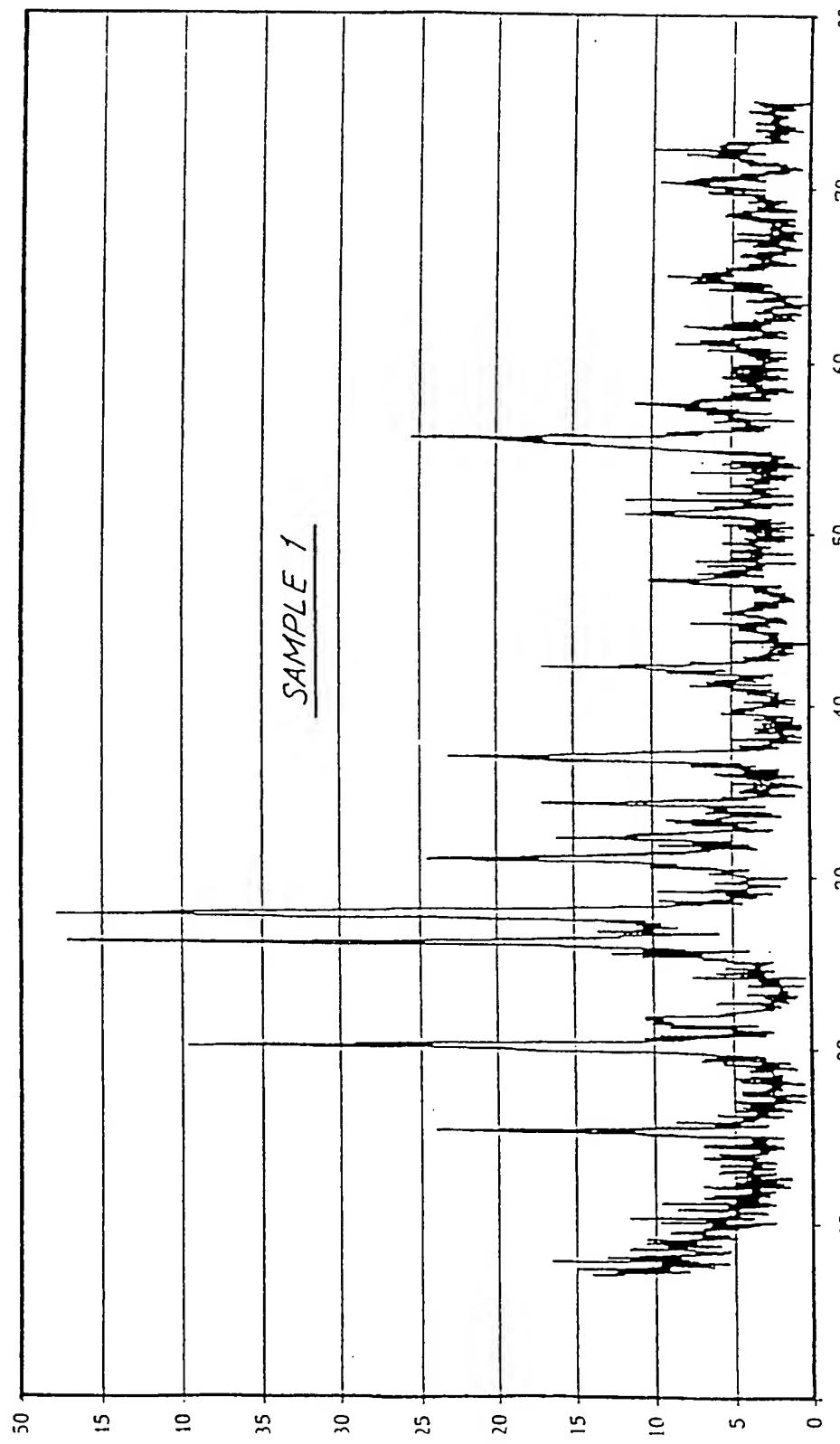
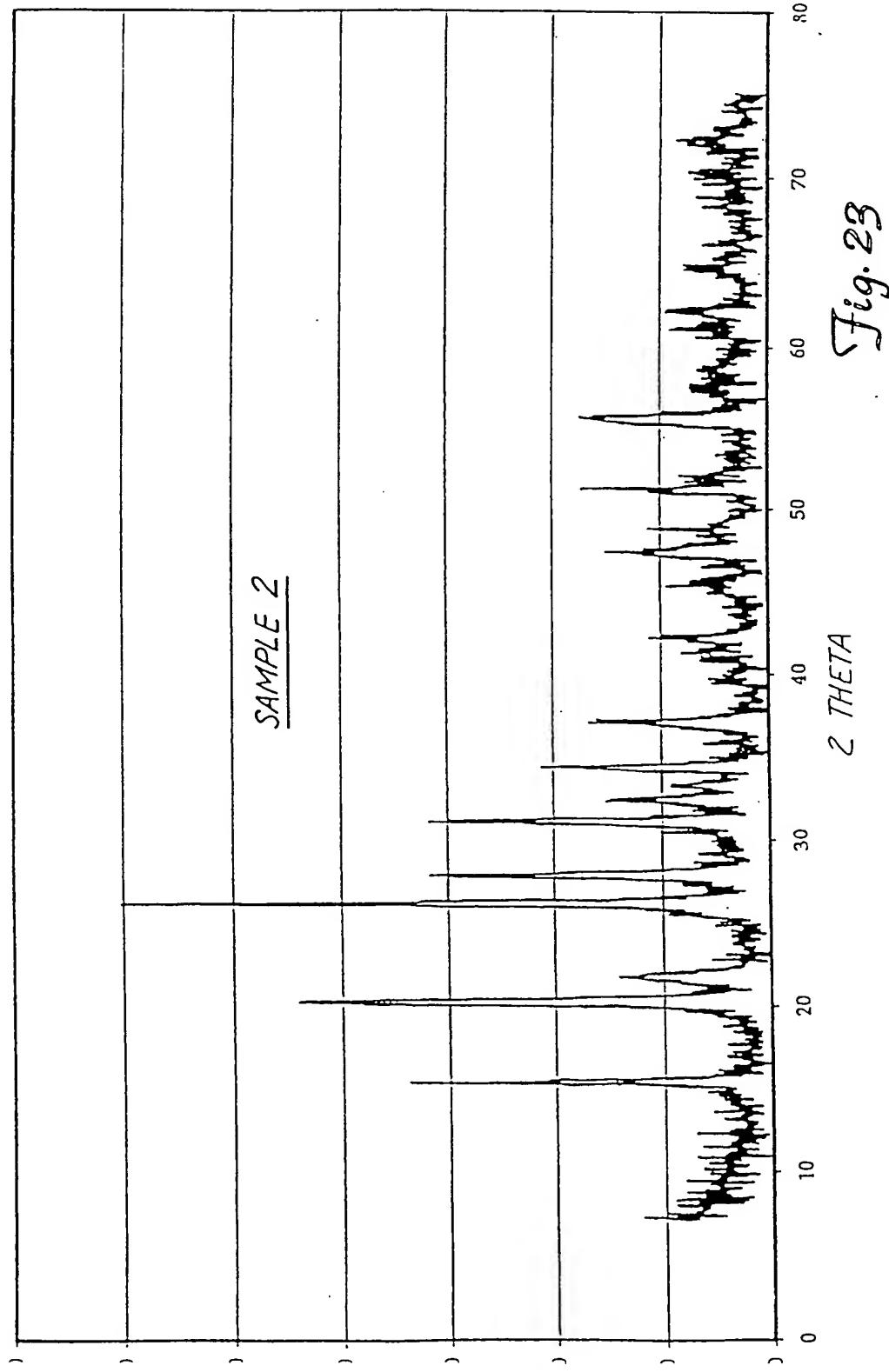


Fig. 22  
2 THETA

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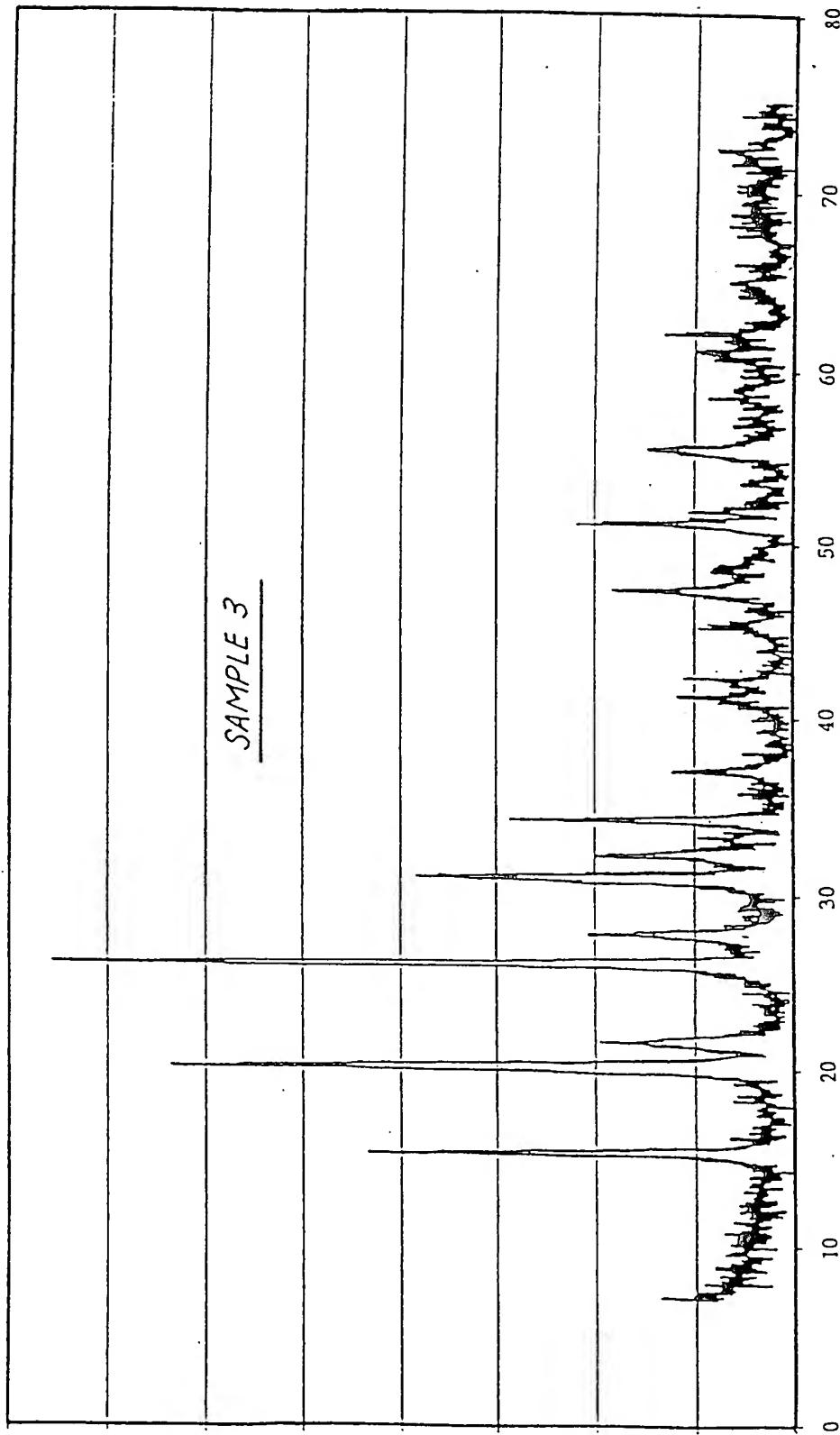


Fig. 24

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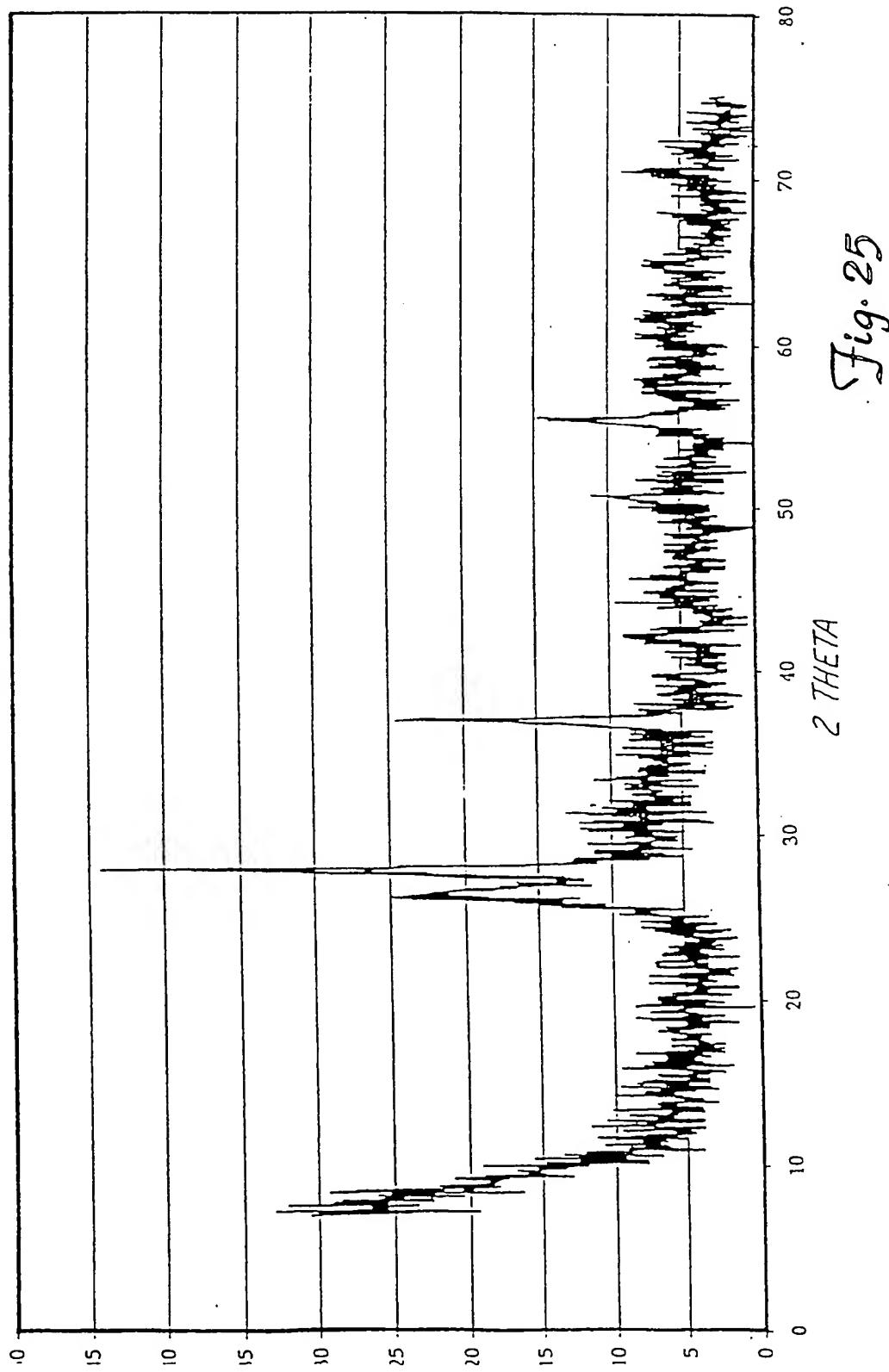


Fig. 25

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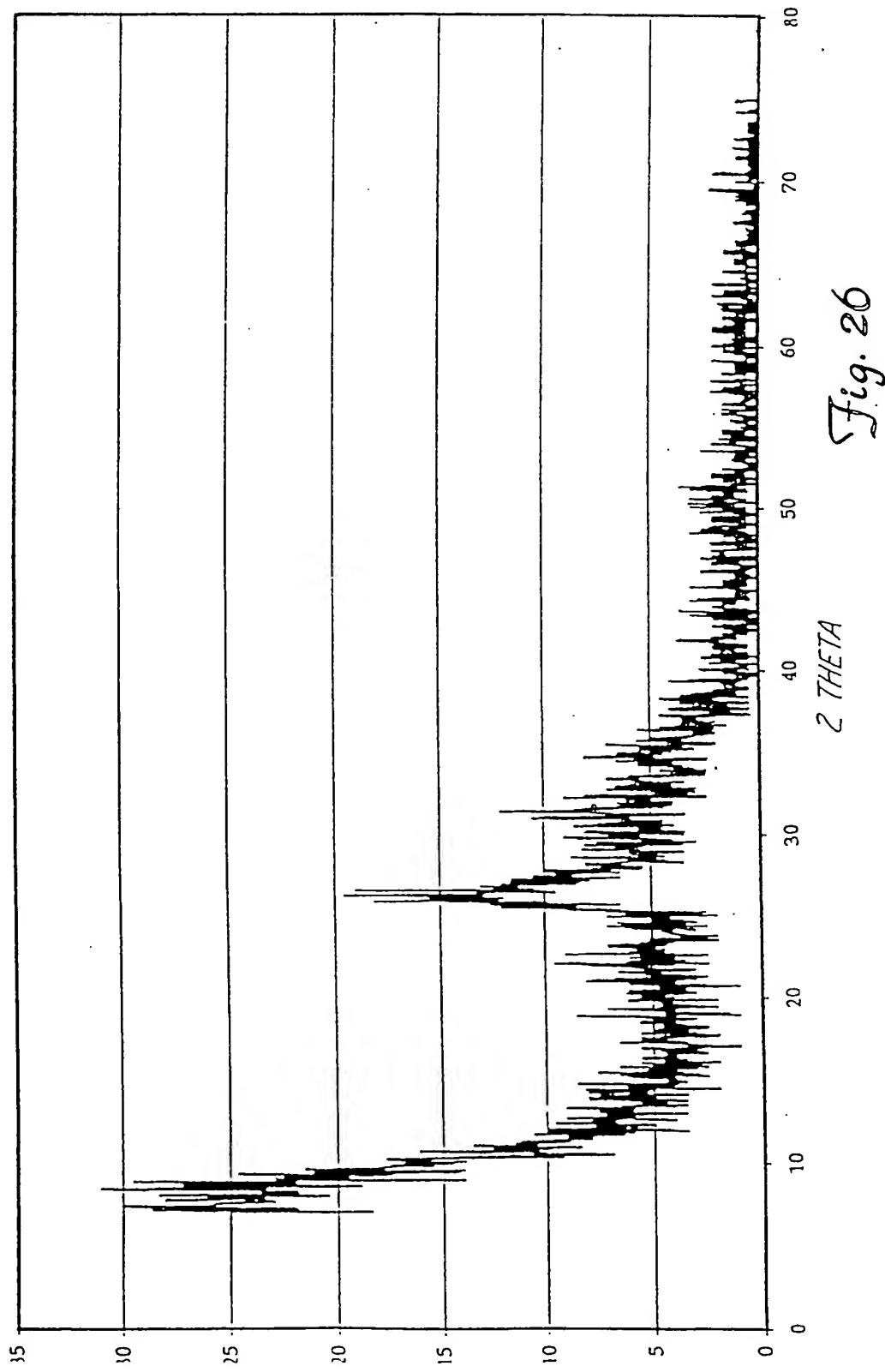
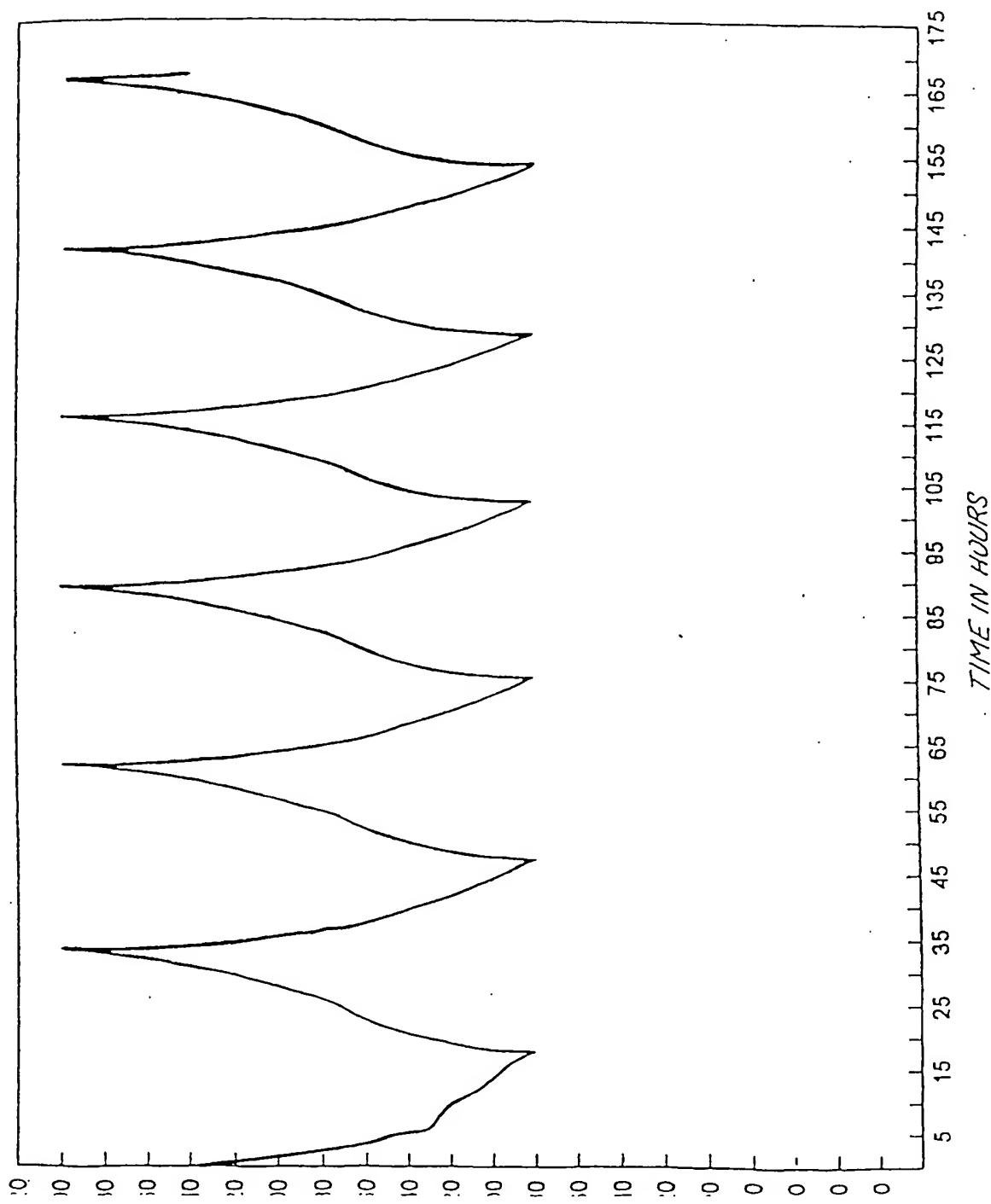
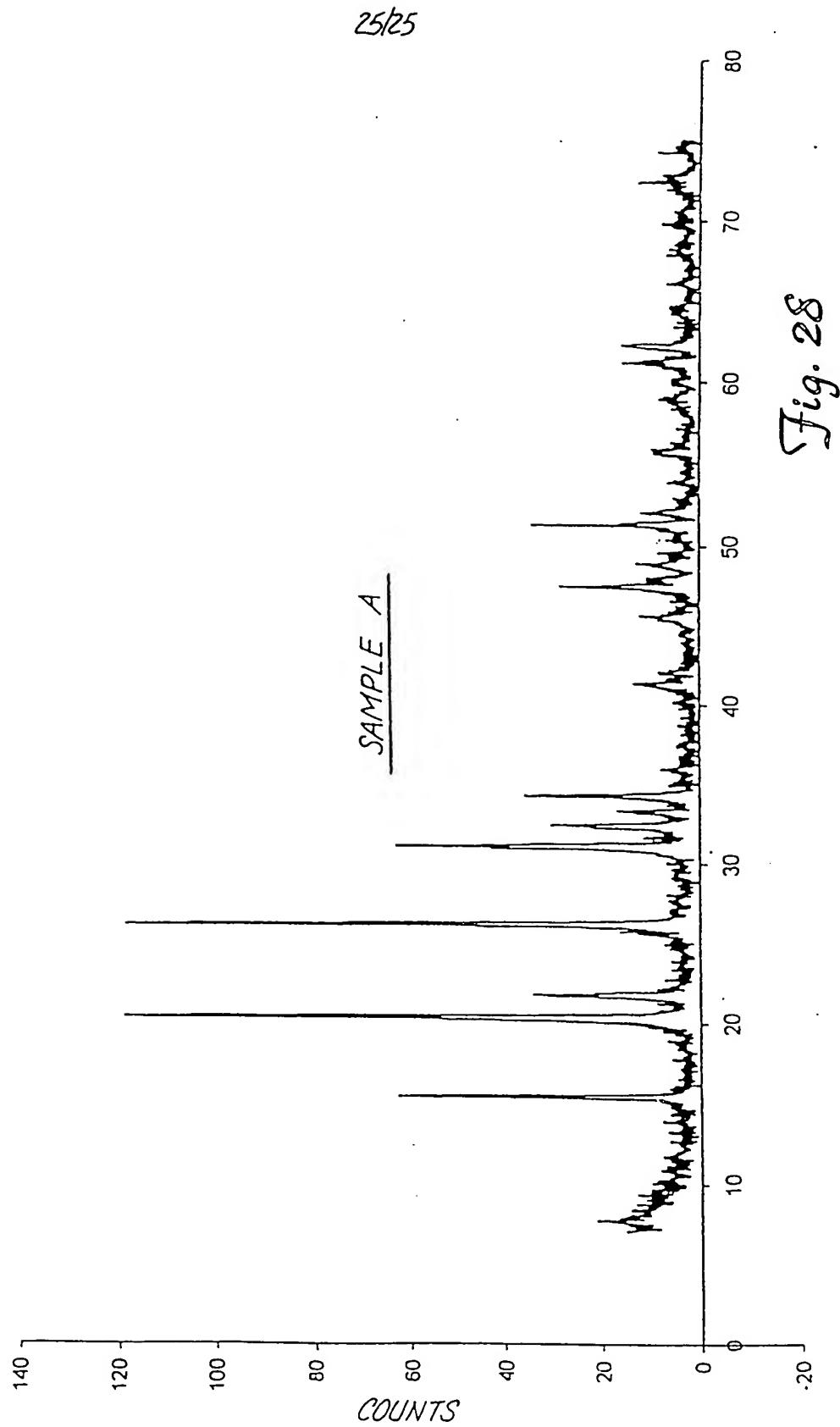


Fig. 26  
2 THETA

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Fig. 27





## INTERNATIONAL SEARCH REPORT

International application No.  
PCT/US98/14947

## A. CLASSIFICATION OF SUBJECT MATTER

IPC(6) :H01M 4/48

US CL :429/231.2; 423/62,579; 149/37; 419/31; 264/28.

According to International Patent Classification (IPC) or to both national classification and IPC

## B. FIELDS SEARCHED

Minimum documentation searched (classification system followed by classification symbols)

U.S. : 429/231.2; 423/62,579; 149/37; 419/31; 264/28.

Documentation searched other than minimum documentation to the extent that such documents are included in the fields searched

Electronic data base consulted during the international search (name of data base and, where practicable, search terms used)

APS, STN (files WPIDS, CA

search terms: vanadium oxides, particle size distribution, nanoparticles, batteries, cathodes

## C. DOCUMENTS CONSIDERED TO BE RELEVANT

Category <sup>a</sup>	Citation of document, with indication, where appropriate, of the relevant passages	Relevant to claim No.
X	US 3,483,110 A (ROZGONYI) 09 December 1969, col. 4, lines 29-42.	14-28
X	US 5,589,300 A (FAUTEUX et al.) 31 December 1996, col. 2, lines 54-63; col. 4, lines 53-59; col. 5, lines 58-61; col. 7, lines 57-63.	1-10
X	US 5,549,880 A (KOKSBANG et al.) 27 August 1996, col. 5, lines 4-6; col. 6, lines 4-35.	1-8 and 29-41
Y	US 5,437,943 A (FUJII et al.) 01 August 1995, col. 5, lines 62-68; col. 6, lines 11-16.	1-8 and 29-41
Y	US 5,443,800 A (OLSEN) 22 August 1995, col. 4, line 63-col. 5, line 2 and Figure 2.	1-13 and 29-41

 Further documents are listed in the continuation of Box C.

See patent family annex.

• Special categories of cited documents:	"T"	later document published after the international filing date or priority date and not in conflict with the application but cited to understand the principle or theory underlying the invention
*A* document defining the general state of the art which is not considered to be of particular relevance	"X"	document of particular relevance; the claimed invention differs from it as considered novel or cannot be considered to involve an inventive step when the document is taken alone
*L* document which may throw doubts on priority claim(s) or which is cited to establish the publication date of another citation or other special reason (as specified)	"Y"	document of particular relevance; the claimed invention involves an inventive step when it is combined with one or more other such documents, such combination being obvious to a person skilled in the art
*O* document referring to an oral disclosure, use, exhibition or other means	"A"	document member of the same patent family
*P* document published prior to the international filing date but later than the priority date claimed		

Date of the actual completion of the international search

07 OCTOBER 1998

Date of mailing of the international search report

10 NOV 1998

## INTERNATIONAL SEARCH REPORT

International application No.  
PCT/US98/14947

### Box I Observations where certain claims were found unsearchable (Continuation of item 1 of first sheet)

This international report has not been established in respect of certain claims under Article 17(2)(a) for the following reasons:

1.  Claims Nos.:  
because they relate to subject matter not required to be searched by this Authority, namely:
  
2.  Claims Nos.:  
because they relate to parts of the international application that do not comply with the prescribed requirements to such an extent that no meaningful international search can be carried out, specifically:
  
3.  Claims Nos.:  
because they are dependent claims and are not drafted in accordance with the second and third sentences of Rule 6.4(a).

### Box II Observations where unity of invention is lacking (Continuation of item 2 of first sheet)

This International Searching Authority found multiple inventions in this international application, as follows:

Please See Extra Sheet.

1.  As all required additional search fees were timely paid by the applicant, this international search report covers all searchable claims.
2.  As all searchable claims could be searched without effort justifying an additional fee, this Authority did not invite payment of any additional fee.
3.  As only some of the required additional search fees were timely paid by the applicant, this international search report covers only those claims for which fees were paid, specifically claims Nos.:
  
4.  No required additional search fees were timely paid by the applicant. Consequently, this international search report is restricted to the invention first mentioned in the claims; it is covered by claims Nos.:

Remark on Protest

The additional search fees were accompanied by the applicant's name.